

STANDARDS OF THE TUBULAR EXCHANGER MANUFACTURERS ASSOCIATION



EIGHTH EDITION

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The Standards herein are recommended by The Tubular Exchanger Manufacturers Association, Inc. to assist users, engineers and designers who specify, design and install tubular exchangers. These standards are based upon sound engineering principles, research and field experience in the manufacture, design, installation and use of tubular exchangers. These standards may be subject to revision as further investigation or experience may show is necessary or desirable. Nothing herein shall constitute a warranty of any kind, expressed or implied, and warranty responsibility of any kind is expressly denied.

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PREFACE

Eighth Edition - 1999

The Eighth Edition of the TEMA Standards was prepared by the Technical Committee of the Tubular Exchanger Manufacturers Association. A compilation of previously proven information, along with new additions to the Flow Induced Vibration, Flexible Shell Elements and Tubesheet Design sections is presented for your practical use.

Design methods for Floating Head Backing Devices have also been added and the scope has been changed to accommodate a larger range of sizes and pressures. Metric units and tables have been included wherever possible. Suggested methods have been included for support and lifting lug design in the RGP section.

This edition of the TEMA Standards is dedicated to the memory of Wayne Schaefer of the Nooter Corporation for his years of dedicated service to the TEMA Technical Committee.

The Editor also wishes to acknowledge the contributions to the Eighth Edition by the following past members of the Technical Committee: Victor J. Stachura, Joseph H. Kissel, Robert C. Moscicki and Harry W. Saultz.

Jim Harrison EDITOR

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NOTES TO USERS OF THE TEMA STANDARDS

Three classes of Mechanical Standards, R, C and B, reflecting acceptable designs for various service applications are presented. The user should refer to the definition of each class and choose the one that best fits the specific need.

Corresponding subject matter in the three Mechanical Standards is covered by paragraphs identically numbered except for the prefix letter. Paragraph numbers preceded by RCB indicates that all three classes are identical. Any reference to a specific paragraph must be preceded by the class designation.

The Recommended Good Practice section has been prepared to assist the designer in areas outside the scope of the basic Standards. Paragraphs in the Standards having additional information in the RGP section are marked with an asterisk (*). The reference paragraph in the RGP section has the identical paragraph number, but with an "RGP" prefix.

It is the intention of the Tubular Exchanger Manufacturers Association that this edition of its Standards may be used beginning with the date of issuance, and that its requirements supersede those of the previous edition six months from such date of issuance, except for heat exchangers contracted for prior to the end of the six month period. For this purpose the date of issuance is June 1, 1999.

Questions on interpretation of the TEMA Standards should be formally addressed to the Secretary at TEMA 25 North Broadway, Tarrytown, NY 10591. Questions requiring development of new or revised technical information will only be answered through an addendum or a new edition of the Standards.

Upon agreement between purchaser and fabricator, exceptions to TEMA requirements are acceptable. An exchanger may still be considered as meeting TEMA requirements as long as the exception is documented.

HIGHLIGHTS OF THE EIGHTH EDITION STANDARDS OF THE Tubular Exchanger Manufacturers Association

The greatly expanded 8th Edition of the Standards of the Tubular Exchanger Manufacturers Association retains the useful data and features found in the Seventh Edition plus many clarifications and innovations. All sections have been reviewed to incorporate new data which were not available at the time of the 1988 printing, including suggestions which resulted from the extensive use of the Standards by both manufacturers and users of shell and tube heat exchangers. Many helpful recommendations were also received through the cooperation of the American Petroleum Institute (API) and the American Society of Mechanical Engineers (ASME).

Some noteworthy features of the Eighth Edition include:

- Metrification has been included where feasible and appropriate.
- Methods for calculating several types of floating head backing rings have been added.
- A method for incorporating pass partition rib area into flange design has been incorporated.
- The vibration section has been expanded and vibration amplitude for vortex shedding and acoustic resonance have been added.
- Nozzle flange pressure/temperature rating tables from ASME Standard B16.5-1996 w/ 1998 addenda are included.
- New materials have been included in coefficient of thermal expansion, modulus of elasticity, and thermal conductivity tables.
- Design equations for double tubesheets have been added.
- A method for calculating the mean metal temperature for tubesheets has been added.
- Stress multipliers have been added to account for the stiffness of knuckles on flanged and flued expansion joints.
- Suggested calculation methods have been incorporated for both vertical and horizontal supports.
- Design methods have been added for lifting lugs.
- A demonstration copy of the available software is included with the purchase of each Standard.

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N-1 SIZE NUMBERING AND TYPE DESIGNATION--RECOMMENDED PRACTICE

It is recommended that heat exchanger size and type be designated by numbers and letters as described below.

N-1.1 SIZE

Sizes of shells (and tube bundles) shall be designated by numbers describing shell (and tube bundle) diameters and tube lengths, as follows:

N-1.11 NOMINAL DIAMETER

The nominal diameter shall be the inside diameter of the shell in inches (mm), rounded off to the nearest integer. For kettle reboilers the nominal diameter shall be the port diameter followed by the shell diameter, each rounded off to the nearest integer.

N-1.12 NOMINAL LENGTH

The nominal length shall be the tube length in inches (mm). Tube length for straight tubes shall be taken as the actual overall length. For U-tubes the length shall be taken as the approximate straight length from end of tube to bend tangent.

N-1.2 TYPE

Type designation shall be by letters describing stationary head, shell (omitted for bundles only), and rear head, in that order, as indicated in Figure N-1.2.

N-1.3 TYPICAL EXAMPLES**N-1.31**

Split-ring floating head exchanger with removable channel and cover, single pass shell, 23-1/4" (591 mm) inside diameter with tubes 16' (4877 mm) long. SIZE 23-192 (591-4877) TYPE AES.

N-1.32

U-tube exchanger with bonnet type stationary head, split flow shell, 19" (483 mm) inside diameter with tubes 7' (2134 mm) straight length. SIZE 19-84 (483-2134) TYPE BGU.

N-1.33

Pull-through floating head kettle type reboiler having stationary head integral with tubesheet, 23" (584 mm) port diameter and 37" (940 mm) inside shell diameter with tubes 16' (4877 mm) long. SIZE 23/37-192 (584/940 - 4877) TYPE CKT.

N-1.34

Fixed tubesheet exchanger with removable channel and cover, bonnet type rear head, two pass shell, 33-1/8" (841 mm) inside diameter with tubes 8' (2438 mm) long. SIZE 33-96 (841-2438) TYPE AFM.

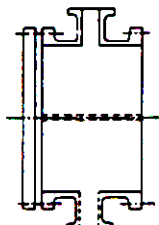
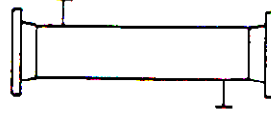
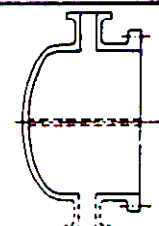
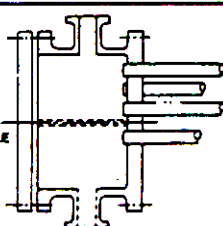
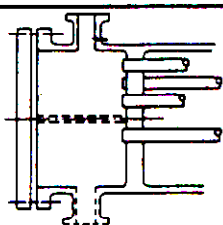
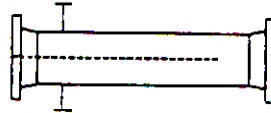
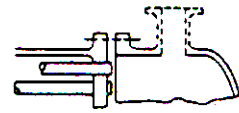
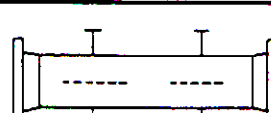
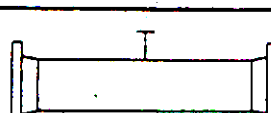
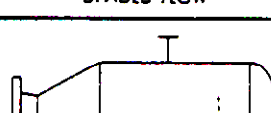
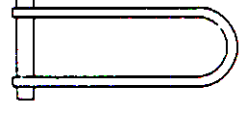
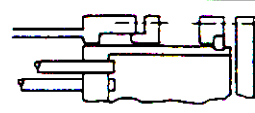
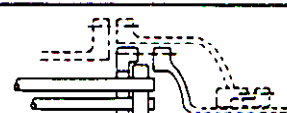
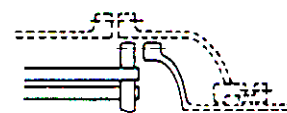
N-1.35

Fixed tubesheet exchanger having stationary and rear heads integral with tubesheets, single pass shell, 17" (432 mm) inside diameter with tubes 16' (4877 mm) long. SIZE 17-192 (432-4877) TYPE NEN.

N-1.4 SPECIAL DESIGNS

Special designs are not covered and may be described as best suits the manufacturer. For example, a single tube pass, fixed tubesheet exchanger with conical heads may be described as "TYPE BEM with Conical Heads". A pull-through floating head exchanger with an integral shell cover may be described as "TYPE AET with Integral Shell Cover".

FIGURE N-1.2

FRONT END STATIONARY HEAD TYPES		SHELL TYPES		REAR END HEAD TYPES	
A		E		L	
	CHANNEL AND REMOVABLE COVER				
					
	BONNET (INTEGRAL COVER)				
					
	REMOVABLE TUBE BUNDLE ONLY				
B		F		M	
	CHANNEL INTEGRAL WITH TUBE- SHEET AND REMOVABLE COVER				
					
	DOUBLE SPLIT FLOW				
					
	DIVIDED FLOW				
C		G		N	
	KETTLE TYPE REBOILER				
					
	CROSS FLOW				
					
	U-TUBE BUNDLE				
D				P	
	EXTERNALLY SEALED FLOATING TUBESHEET				
					
	FLOATING HEAD WITH BACKING DEVICE				
					
	PULL THROUGH FLOATING HEAD				

N-2 NOMENCLATURE OF HEAT EXCHANGER COMPONENTS

For the purpose of establishing standard terminology, Figure N-2 illustrates various types of heat exchangers. Typical parts and connections, for illustrative purposes only, are numbered for identification in Table N-2.

TABLE N-2

1. Stationary Head-Channel	21. Floating Head Cover-External
2. Stationary Head-Bonnet	22. Floating Tubesheet Skirt
3. Stationary Head Flange-Channel or Bonnet	23. Packing Box
4. Channel Cover	24. Packing
5. Stationary Head Nozzle	25. Packing Gland
6. Stationary Tubesheet	26. Lantern Ring
7. Tubes	27. Tierods and Spacers
8. Shell	28. Transverse Baffles or Support Plates
9. Shell Cover	29. Impingement Plate
10. Shell Flange-Stationary Head End	30. Longitudinal Baffle
11. Shell Flange-Rear Head End	31. Pass Partition
12. Shell Nozzle	32. Vent Connection
13. Shell Cover Flange	33. Drain Connection
14. Expansion Joint	34. Instrument Connection
15. Floating Tubesheet	35. Support Saddle
16. Floating Head Cover	36. Lifting Lug
17. Floating Head Cover Flange	37. Support Bracket
18. Floating Head Backing Device	38. Weir
19. Split Shear Ring	39. Liquid Level Connection
20. Slip-on Backing Flange	40. Floating Head Support

FIGURE N-2

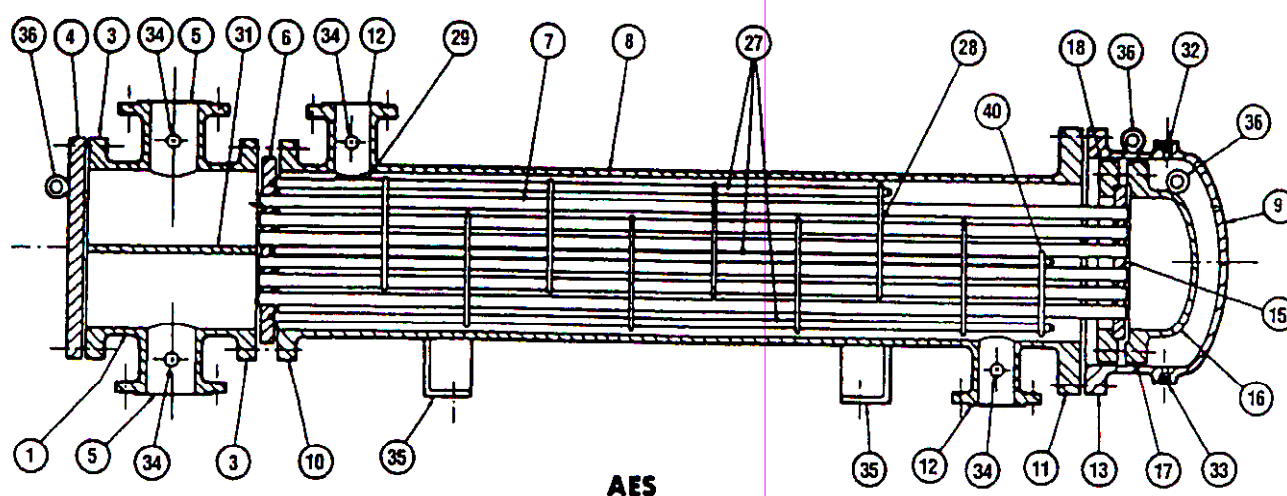


FIGURE N-2 (continued)

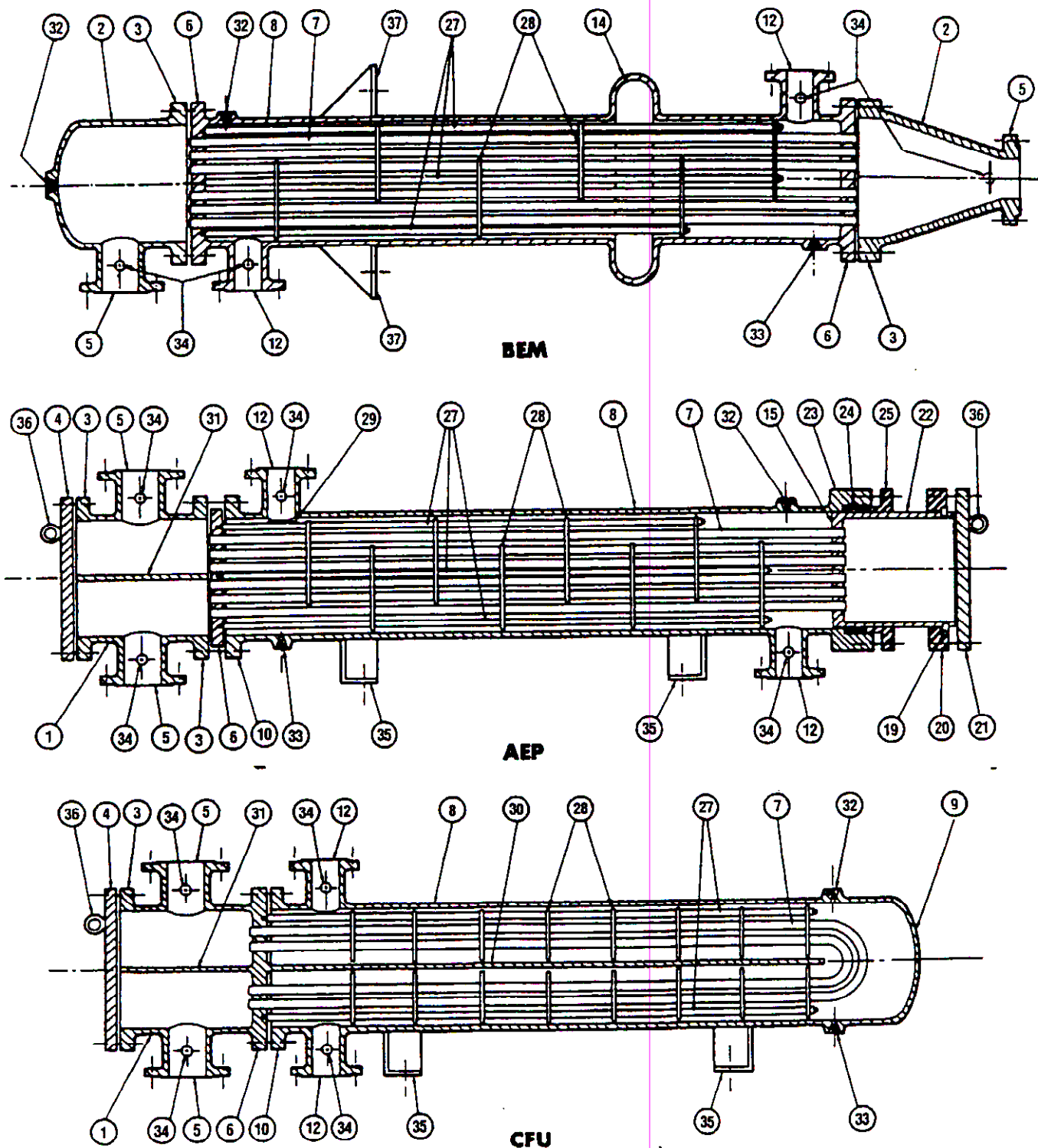
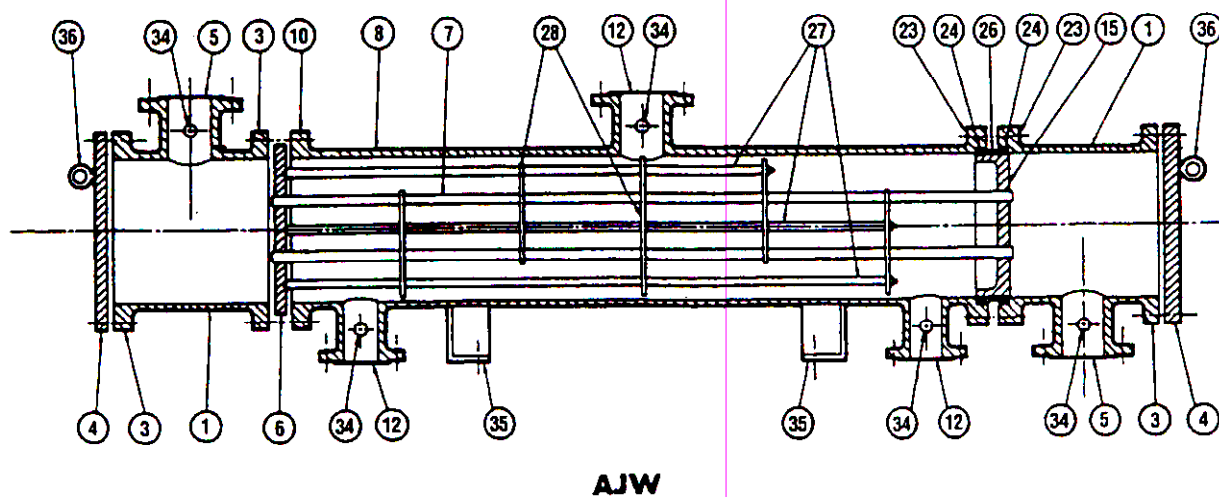
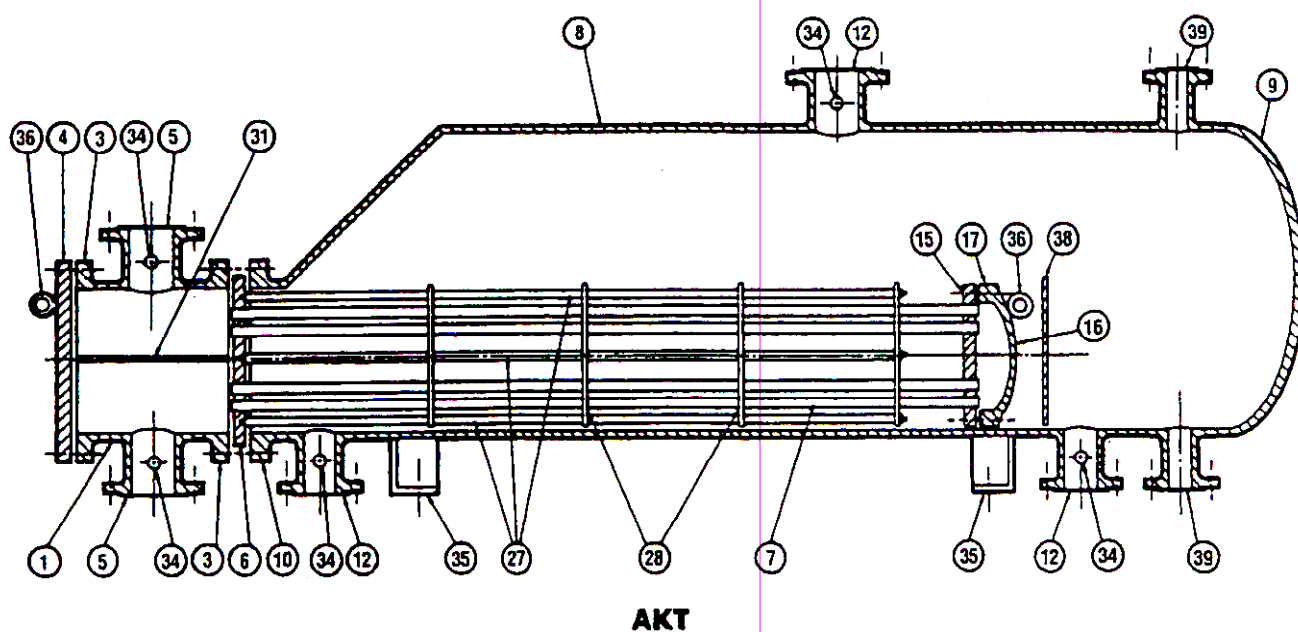


FIGURE N-2 (continued)

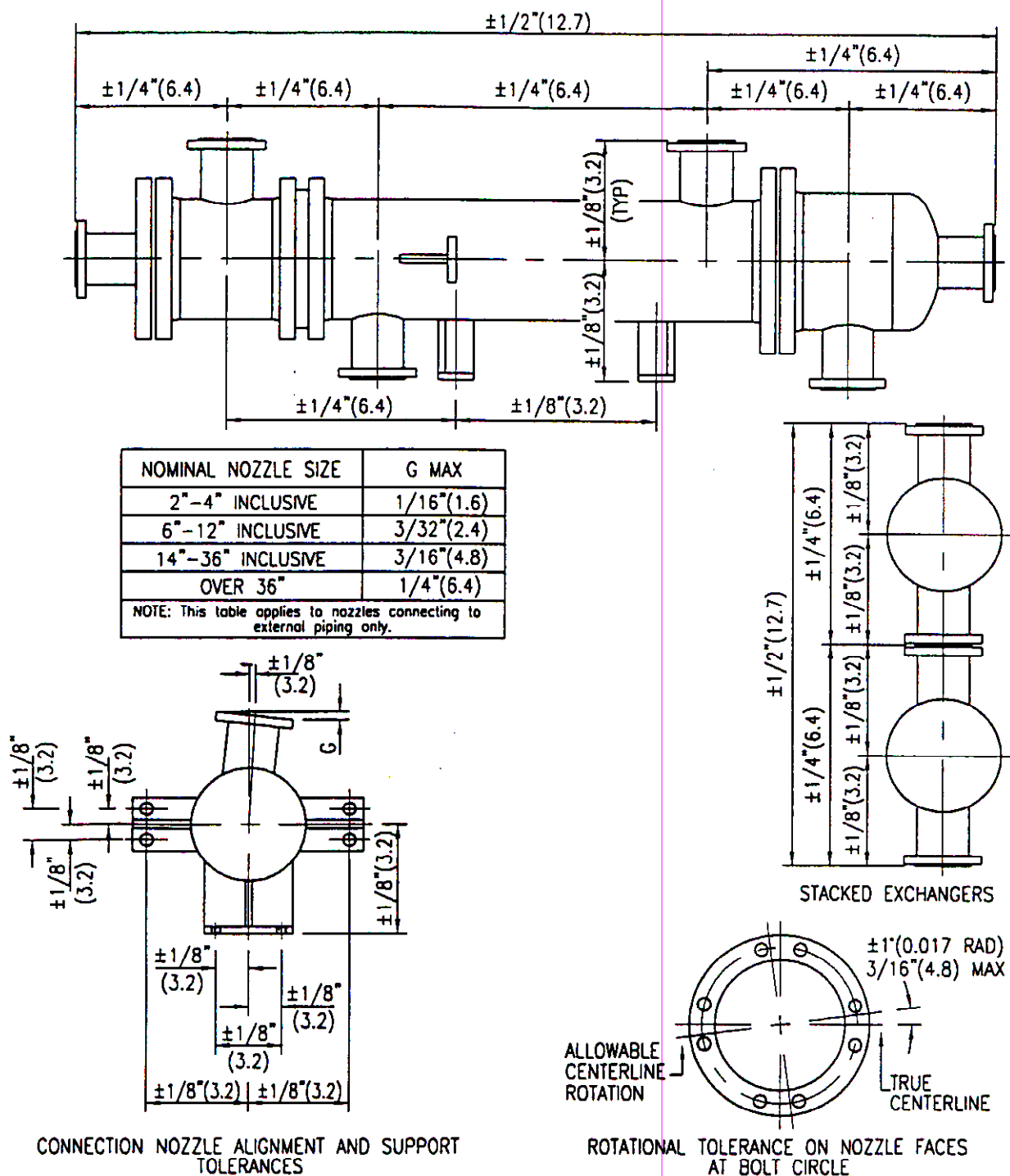


SECTION 2 HEAT EXCHANGER FABRICATION TOLERANCES

F-1 EXTERNAL DIMENSIONS, NOZZLE AND SUPPORT LOCATIONS

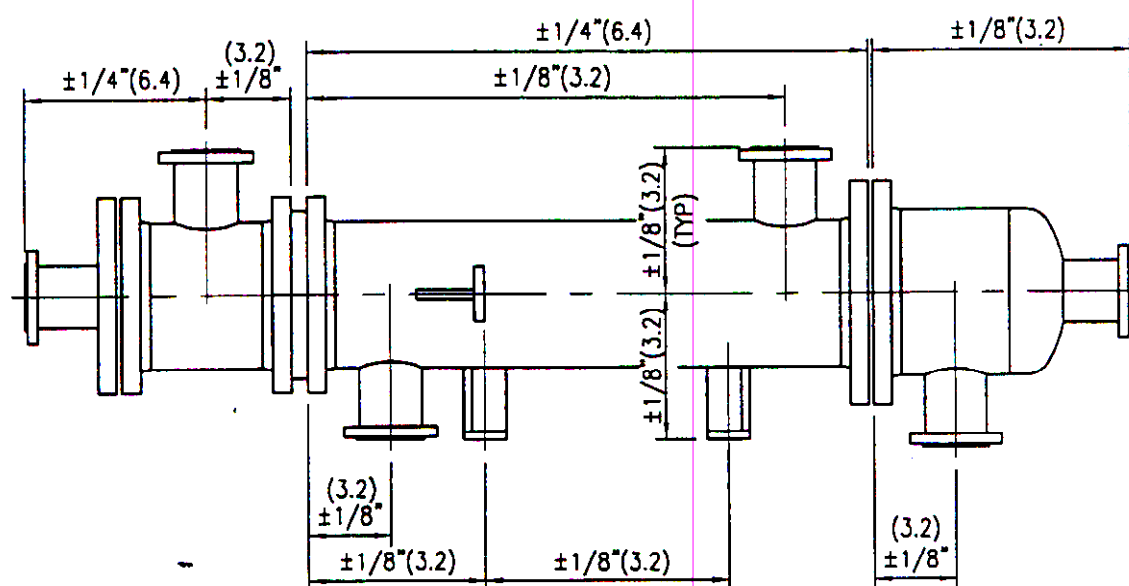
Standard tolerances for process flow nozzles and support locations and projections are shown in Figure F-1. Dimensions in () are millimeters.

FIGURE F-1



F-2 RECOMMENDED FABRICATION TOLERANCES

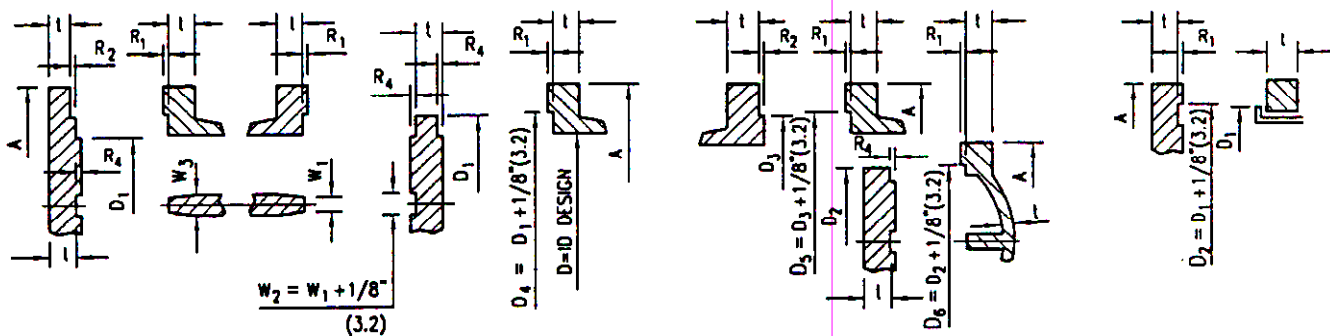
Fabrication tolerances normally required to maintain process flow nozzle and support locations are shown in Figure F-2. These tolerances may be adjusted as necessary to meet the tolerances shown in Figure F-1. Dimensions in () are millimeters.

FIGURE F-2

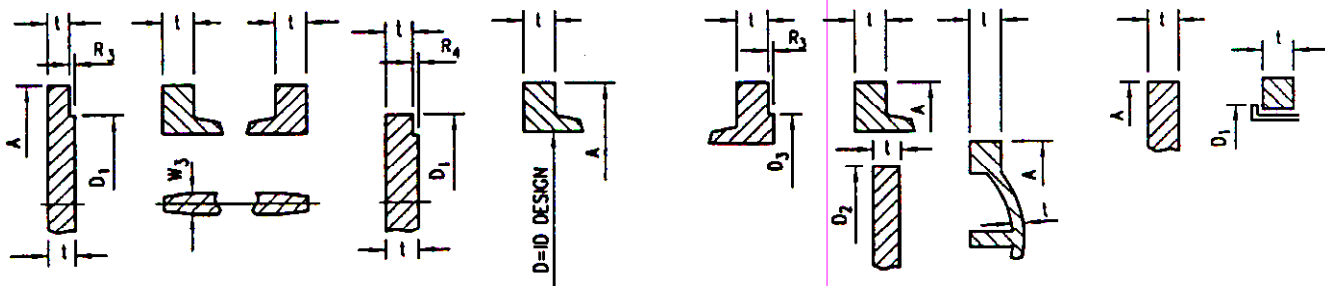
F-3 TUBESHEETS, PARTITIONS, COVERS AND FLANGES

The standard clearances and tolerances applying to tubesheets, partitions, covers and flanges are shown in Figure F-3. Dimensions in () are millimeters.

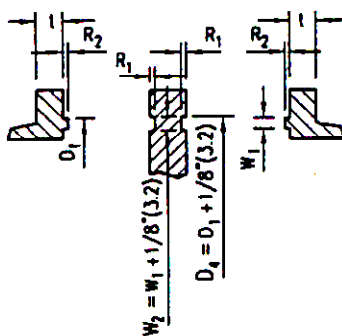
FIGURE F-3



STANDARD CONFINED JOINT CONSTRUCTION



STANDARD UNCONFINED PLAIN FACE JOINT CONSTRUCTION

ALTERNATE
TONGUE AND GROOVE
JOINT

DIMENSIONS	TOLERANCES
A	$+1/4^{\circ} -1/8^{\circ}$ (+6.4 -3.2)
D ₁ , D ₂ , D ₃ , D ₄ , D ₅ , D ₆	$\pm 1/32^{\circ}$ (± 0.8)
t	$\pm 1/16^{\circ}$ (± 1.6)
R ₁ = 3/16" (4.8)	$+0^{\circ} -1/32^{\circ}$ (+0 -0.8)
R ₂ = 1/4" (6.4) R ₃ = 1/4" (6.4)	$+1/32^{\circ} -0^{\circ}$ (+0.8 -0)
R ₄ = 3/16" (4.8)	$-1/32^{\circ} (-0.8)$ (SEE NOTE 1)
W ₁ , W ₂ , W ₃	$\pm 1/32^{\circ}$ (± 0.8)

1. SECTION 2 IS NOT INTENDED TO PROHIBIT UNMACHINED TUBESHEET FACES AND FLAT COVER FACES. THEREFORE NO PLUS TOLERANCE IS SHOWN ON R₄.

2. NEGATIVE TOLERANCES SHALL NOT BE CONSTRUED TO MEAN THAT FINAL DIMENSIONS CAN BE LESS THAN THAT REQUIRED BY DESIGN CALCULATIONS.

3. FOR PERIPHERAL GASKETS, "CONFINED" MEANS "CONFINED ON THE OD".

4. DETAILS ARE TYPICAL AND DO NOT PRECLUDE THE USE OF OTHER DETAILS WHICH ARE FUNCTIONALLY EQUIVALENT.

5. FOR UNITS OVER 60" (1524) TO 100" (2540) DIAMETER, TOLERANCES "D" AND "W" MAY BE INCREASED TO $\pm 1/16^{\circ}$ (1.6).

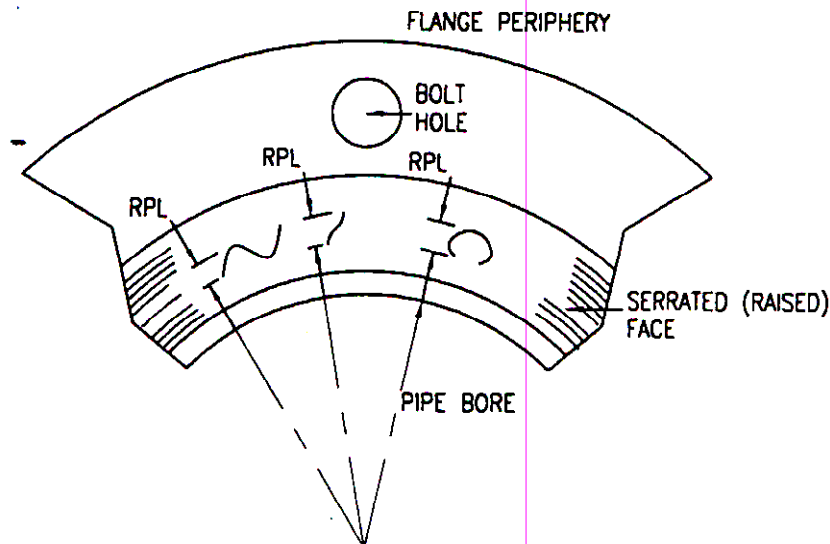
FIGURE F-4

PERMISSIBLE IMPERFECTIONS IN FLANGE FACING FINISH
FOR RAISED FACE AND LARGE MALE AND FEMALE FLANGES 1,2

NPS	Maximum Radial Projection of Imperfections Which Are No Deeper Than the Bottom of the Serrations, in. (mm)	Maximum Depth and Radial Projection of Imperfections Which Are Deeper Than the Bottom of the Serrations, in. (mm)
1/2	1/8 (3.2)	1/16 (1.6)
3/4	1/8 (3.2)	1/16 (1.6)
1	1/8 (3.2)	1/16 (1.6)
1-1/4	1/8 (3.2)	1/16 (1.6)
1-1/2	1/8 (3.2)	1/16 (1.6)
2	1/8 (3.2)	1/16 (1.6)
2-1/2	1/8 (3.2)	1/16 (1.6)
3	3/16 (4.8)	1/16 (1.6)
3-1/2	1/4 (6.4)	1/8 (3.2)
4	1/4 (6.4)	1/8 (3.2)
5	1/4 (6.4)	1/8 (3.2)
6	1/4 (6.4)	1/8 (3.2)
8	5/16 (7.9)	1/8 (3.2)
10	5/16 (7.9)	3/16 (4.8)
12	5/16 (7.9)	3/16 (4.8)
14	5/16 (7.9)	3/16 (4.8)
16	3/8 (9.5)	3/16 (4.8)
18	1/2 (12.7)	1/4 (6.4)
20	1/2 (12.7)	1/4 (6.4)
24	1/2 (12.7)	1/4 (6.4)

NOTES:

- (1) Imperfections must be separated by at least four times the permissible radial projection.
- (2) Protrusions above the serrations are not permitted.



Sketch showing Radial Projected Length (RPL) serrated gasket face damage

DEFINITIONS

1. Baffle is a device to direct the shell side fluid across the tubes for optimum heat transfer.
2. Baffle and Support Plate Tube Hole Clearance is the diametral difference between the nominal tube OD and the nominal tube hole diameter in the baffle or support plate.
3. Consequential Damages are indirect liabilities lying outside the heat exchanger manufacturer's stated equipment warranty obligations.
4. Double Tubesheet Construction is a type of construction in which two (2) spaced tubesheets or equivalent are employed in lieu of the single tubesheet at one or both ends of the heat exchanger.
5. Effective Shell and Tube Side Design Pressures are the resultant load values expressed as uniform pressures used in the determination of tubesheet thickness for fixed tubesheet heat exchangers and are functions of the shell side design pressure, the tube side design pressure, the equivalent differential expansion pressure and the equivalent bolting pressure.
6. Equivalent Bolting Pressure is the pressure equivalent resulting from the effects of bolting loads imposed on tubesheets in a fixed tubesheet heat exchanger when the tubesheets are extended for bolting as flanged connections.
7. Equivalent Differential Expansion Pressure is the pressure equivalent resulting from the effect of tubesheet loadings in a fixed tubesheet heat exchanger imposed by the restraint of differential thermal expansion between shell and tubes.
8. Expanded Tube Joint is the tube-to-tubesheet joint achieved by mechanical or explosive expansion of the tube into the tube hole in the tubesheet.
9. Expansion Joint "J" Factor is the ratio of the spring rate of the expansion joint to the sum of the axial spring rate of the shell and the spring rate of the expansion joint.
10. Flange Load Concentration Factors are factors used to compensate for the uneven application of bolting moments due to large bolt spacing.
11. Minimum and Maximum Baffle and Support Spacings are design limitations for the spacing of baffles to provide for mechanical integrity and thermal and hydraulic effectiveness of the bundle. The possibility for induced vibration has not been considered in establishing these values.
12. Normal Operating Conditions of a shell and tube heat exchanger are the thermal and hydraulic performance requirements generally specified for sizing the heat exchanger.
13. Pulsating Fluid Conditions are conditions of flow generally characterized by rapid fluctuations in pressure and flow rate resulting from sources outside of the heat exchanger.
14. Seismic Loadings are forces and moments resulting in induced stresses on any member of a heat exchanger due to pulse mode or complex waveform accelerations to the heat exchanger, such as those resulting from earthquakes.
15. Shell and Tube Mean Metal Temperatures are the average metal temperatures through the shell and tube thicknesses integrated over the length of the heat exchanger for a given steady state operating condition.
16. Shut-Down Conditions are the conditions of operation which exist from the time of steady state operating conditions to the time that flow of both process streams has ceased.
17. Start-Up Conditions are the conditions of operation which exist from the time that flow of either or both process streams is initiated to the time that steady state operating conditions are achieved.
18. Support plate is a device to support the bundle or to reduce unsupported tube span without consideration for heat transfer.
19. Tubesheet Ligament is the shortest distance between edge of adjacent tube holes in the tube pattern.
20. Welded Tube Joint is a tube-to-tubesheet joint where the tube is welded to the tubesheet.

**FIGURE G-5.2
HEAT EXCHANGER SPECIFICATION SHEET**

1					Job No.	
2	Customer				Reference No.	
3	Address				Proposal No.	
4	Plant Location				Date	Rev.
5	Service of Unit				Item No.	
6	Size	Type	(Hor/Vert)	Connected in	Parallel	Series
7	Surf/Unit (Gross/Eff.)	Sq Ft; Shells/Unit		Surf/Shell (Gross/Eff.)	Sq Ft	
8	PERFORMANCE OF ONE UNIT					
9	Fluid Allocation		Shell Side		Tube Side	
10	Fluid Name					
11	Fluid Quantity Total		Lb/Hr			
12	Vapor (In/Out)					
13	Liquid					
14	Steam					
15	Water					
16	Noncondensable					
17	Temperature (In/Out)		°F			
18	Specific Gravity					
19	Viscosity, Liquid		Cp			
20	Molecular Weight, Vapor					
21	Molecular Weight, Noncondensable					
22	Specific Heat		Btu / Lb °F			
23	Thermal Conductivity		Btu Ft / Hr Sq Ft °F			
24	Latent Heat		Btu / Lb @ °F			
25	Inlet Pressure		Psia			
26	Velocity		Ft / Sec			
27	Pressure Drop, Allow. /Calc.		Psi			
28	Fouling Resistance (Min.)		Hr Sq Ft °F / Btu			
29	Heat Exchanged		Btu / Hr; MTD (Corrected) °F			
30	Transfer Rate, Service		Clean Btu / Hr Sq Ft °F			
31	CONSTRUCTION OF ONE SHELL					
32			Shell Side		Tube Side	
33	Design / Test Pressure		Psig		/	
34	Design Temp. Max/Min		°F		/	
35	No. Passes per Shell					
36	Corrosion Allowance		In			
37	Connections		In			
38	Size & Rating		Out			
39			Intermediate			
40	Tube No.	OD	In; Thk (Min/Avg)	In; Length	Ft; Pitch	In 30 60 90 45
41	Tube Type		Material			
42	Shell	ID	OD	In	Shell Cover	(Integ.) (Remov.)
43	Channel or Bonnet			Channel Cover		
44	Tubesheet-Stationary			Tubesheet-Floating		
45	Floating Head Cover			Impingement Protection		
46	Baffles-Cross	Type	%Cut (Diam/Area)		Spacing: c/c	Inlet In
47	Baffles-Long	Seal Type				
48	Supports-Tube	U-Bend	Type			
49	Bypass Seal Arrangement		Tube-to-Tubesheet Joint			
50	Expansion Joint		Type			
51	pV-Inlet Nozzle	Bundle Entrance		Bundle Exit		
52	Gaskets-Shell Side		Tube Side			
53	Floating Head					
54	Code Requirements		TEMA Class			
55	Weight / Shell	Filled with Water		Bundle Lb		
56	Remarks					
57						
58						
59						
60						
61						

SECTION 3 GENERAL FABRICATION AND PERFORMANCE INFORMATION

FIGURE G-5.2M
HEAT EXCHANGER SPECIFICATION SHEET

1					Job No.	
2	Customer				Reference No.	
3	Address				Proposal No.	
4	Plant Location				Date	Rev.
5	Service of Unit				Item No.	
6	Size	Type	(Hor/Vert)	Connected in	Parallel	Series
7	Surf/Unit (Gross/Eff.)	Sq m; Shells/Unit		Surf/Shell (Gross/Eff.)	Sq m	
8	PERFORMANCE OF ONE UNIT					
9	Fluid Allocation			Shell Side		Tube Side
10	Fluid Name					
11	Fluid Quantity Total			kg/Hr		
12	Vapor (In/Out)					
13	Liquid					
14	Steam					
15	Water					
16	Noncondensable					
17	Temperature (In/Out)			°C		
18	Specific Gravity					
19	Viscosity, Liquid			Cp		
20	Molecular Weight, Vapor					
21	Molecular Weight, Noncondensable					
22	Specific Heat			J/kg °C		
23	Thermal Conductivity			W/m °C		
24	Latent Heat			J/kg @ °C		
25	Inlet Pressure			kPa(abs.)		
26	Velocity			m/sec		
27	Pressure Drop, Allow. /Calc.			kPa		/
28	Fouling Resistance (Min.)			Sq m °C / W		
29	Heat Exchanged			W:MTD (Corrected)		°C
30	Transfer Rate, Service			Clean		W/Sq m °C
31	CONSTRUCTION OF ONE SHELL					Sketch (Bundle/Nozzle Orientation)
32				Shell Side	Tube Side	
33	Design / Test Pressure	kPag	/	/	/	
34	Design Temp. Max/Min	°C	/	/	/	
35	No. Passes per Shell					
36	Corrosion Allowance	mm				
37	Connections	In				
38	Size & Rating	Out				
39		Intermediate				
40	Tube No.	OD	mm;Thk (Min/Avg)	mm;Length	mm;Pitch	mm ← 30 → 60 → 90 → 45
41	Tube Type					
42	Shell	ID	OD	mm	Shell Cover	(Integ.) (Remov.)
43	Channel or Bonnet				Channel Cover	
44	Tubesheet-Stationary				Tubesheet-Floating	
45	Floating Head Cover				Impingement Protection	
46	Baffles-Cross	Type	%Cut (Diam/Area)		Spacing: c/c	Inlet mm
47	Baffles-Long	Seal Type				
48	Supports-Tube	U-Bend	Type			
49	Bypass Seal Arrangement				Tube-to-Tubesheet Joint	
50	Expansion Joint				Type	
51	pV'-Inlet Nozzle	Bundle Entrance		Bundle Exit		
52	Gaskets-Shell Side	Tube Side				
53	Floating Head					
54	Code Requirements				TEMA Class	
55	Weight / Shell	Filled with Water		Bundle		kg
56	Remarks					
57						
58						
59						
60						
61						

G-1 SHOP OPERATION

The detailed methods of shop operation are left to the discretion of the manufacturer in conformity with these Standards.

G-2 INSPECTION**G-2.1 MANUFACTURER'S INSPECTION**

Inspection and testing of units will be provided by the manufacturer unless otherwise specified. The manufacturer shall carry out the inspections required by the ASME Code, and also inspections required by state and local codes when the purchaser specifies the plant location.

G-2.2 PURCHASER'S INSPECTION

The purchaser shall have the right to make inspections during fabrication and to witness any tests when he has so requested. Advance notification shall be given as agreed between the manufacturer and the purchaser. Inspection by the purchaser shall not relieve the manufacturer of his responsibilities.

G-3 NAME PLATES**G-3.1 MANUFACTURER'S NAME PLATE**

A suitable manufacturer's name plate of corrosion resistant material shall be permanently attached to the head end or the shell of each TEMA exchanger. Name plates for exchangers manufactured in accordance with Classes "R" and "B" shall be austenitic (300 series) stainless. When insulation thickness is specified by the purchaser, the name plate shall be attached to a bracket welded to the exchanger.

G-3.11 NAME PLATE DATA

In addition to all data required by the ASME Code, a name plate shall also include the following (if provided):

User's equipment identification
User's order number

G-3.12 SUPPLEMENTAL INFORMATION

The manufacturer shall supply supplemental information where it is pertinent to the operation or testing of the exchanger. This would include information pertaining to differential design and test pressure conditions, restrictions on operating conditions for fixed tubesheet type exchangers, or other restrictive conditions applicable to the design and/or operation of the unit or its components. Such information can be noted on the name plate or on a supplemental plate attached to the exchanger at the name plate location.

G-3.2 PURCHASER'S NAME PLATE

Purchaser's name plates, when used, are to be supplied by the purchaser and supplement rather than replace the manufacturer's name plate.

G-3.3 TEMA REGISTRATION PLATE

The TEMA organization has adopted a voluntary registration system for TEMA members only. When a heat exchanger is registered with TEMA, a unique number is assigned to the heat exchanger. A TEMA registration plate, showing this number, is affixed to the heat exchanger and the ASME Code data report is placed on file at the TEMA office. By referencing this registration number, a copy of the ASME Code data report may be obtained by the purchaser from the TEMA office.

G-4 DRAWINGS AND ASME CODE DATA REPORTS**G-4.1 DRAWINGS FOR APPROVAL AND CHANGE**

The manufacturer shall submit for purchaser's approval three (3) prints of an outline drawing showing nozzle sizes and locations, overall dimensions, supports and weight. Other drawings may be furnished as agreed upon by the purchaser and the manufacturer. It is anticipated that a reasonable number of minor drawing changes may be required at that time. Changes subsequent to receipt of approval may cause additional expense chargeable to the purchaser. Purchaser's approval of drawings does not relieve the manufacturer of responsibility for compliance with this Standard and applicable ASME Code requirements. The manufacturer shall not make any changes

SECTION 3 GENERAL FABRICATION AND PERFORMANCE INFORMATION

on the approved drawings without express agreement of the purchaser. Shop detail drawings, while primarily for internal use by the fabricator, may be furnished to the purchaser upon request. When detail drawings are requested, they will only be supplied after outline drawings have been approved.

G-4.2 DRAWINGS FOR RECORD

After approval of drawings, the manufacturer shall furnish three (3) prints or, at his option, a transparency of all approved drawings.

G-4.3 PROPRIETARY RIGHTS TO DRAWINGS

The drawings and the design indicated by them are to be considered the property of the manufacturer and are not to be used or reproduced without his permission, except by the purchaser for his own internal use.

G-4.4 ASME CODE DATA REPORTS

After completion of fabrication and inspection of ASME Code stamped exchangers, the manufacturer shall furnish three (3) copies of the ASME Manufacturer's Data Report.

G-5 GUARANTEES

G-5.1 GENERAL

The specific terms of the guarantees should be agreed upon by the manufacturer and purchaser. Unless otherwise agreed upon by the manufacturer and purchaser, the following paragraphs in this section will be applicable.

G-5.2 PERFORMANCE

The purchaser shall furnish the manufacturer with all information needed for clear understanding of performance requirements, including any special requirements. The manufacturer shall guarantee thermal performance and mechanical design of a heat exchanger, when operated at the design conditions specified by the purchaser in his order, or shown on the exchanger specification sheet furnished by the manufacturer (Figure G-5.2, G-5.2M). This guarantee shall extend for a period of twelve (12) months after shipping date. The manufacturer shall assume no responsibility for excessive fouling of the apparatus by material such as coke, silt, scale, or any foreign substance that may be deposited. The thermal guarantee shall not be applicable to exchangers where the thermal performance rating was made by the purchaser.

G-5.21 THERMAL PERFORMANCE TEST

A performance test shall be made if it is established after operation that the performance of the exchanger is not satisfactory, provided the thermal performance rating was made by the manufacturer. Test conditions and procedures shall be selected by agreement between the purchaser and the manufacturer to permit extrapolation of the test results to the specified design conditions.

G-5.22 DEFECTIVE PARTS

The manufacturer shall repair or replace F.O.B. his plant any parts proven defective within the guarantee period. Finished materials and accessories purchased from other manufacturers, including tubes, are warranted only to the extent of the original manufacturer's warranty to the heat exchanger fabricator.

G-5.3 CONSEQUENTIAL DAMAGES

The manufacturer shall not be held liable for any indirect or consequential damage.

G-5.4 CORROSION AND VIBRATION

The manufacturer assumes no responsibility for deterioration of any part or parts of the equipment due to corrosion, erosion, flow induced tube vibration, or any other causes, regardless of when such deterioration occurs after leaving the manufacturer's premises, except as provided for in Paragraphs G-5.2 and G-5.22.

G-5.5 REPLACEMENT AND SPARE PARTS

When replacement or spare tube bundles, shells, or other parts are purchased, the manufacturer is to guarantee satisfactory fit of such parts only if he was the original manufacturer. Parts fabricated to drawings furnished by the purchaser shall be guaranteed to meet the dimensions and tolerances specified.

G-6 PREPARATION OF HEAT EXCHANGERS FOR SHIPMENT**G-6.1 CLEANING**

Internal and external surfaces are to be free from loose scale and other foreign material that is readily removable by hand or power brushing.

G-6.2 DRAINING

Water, oil, or other liquids used for cleaning or hydrostatic testing are to be drained from all units before shipment. This is not to imply that the units must be completely dry.

G-6.3 FLANGE PROTECTION

All exposed machined contact surfaces shall be coated with a removable rust preventative and protected against mechanical damage by suitable covers.

G-6.4 THREADED CONNECTION PROTECTION

All threaded connections are to be suitably plugged.

G-6.5 DAMAGE PROTECTION

The exchanger and any spare parts are to be suitably protected to prevent damage during shipment.

G-6.6 EXPANSION JOINT PROTECTION

External thin walled expansion bellows shall be equipped with a protective cover which does not restrain movement.

G-7 GENERAL CONSTRUCTION FEATURES OF TEMA STANDARD HEAT EXCHANGERS**G-7.1 SUPPORTS**

All heat exchangers are to be provided with supports.

***G-7.11 HORIZONTAL UNITS**

The supports should be designed to accommodate the weight of the unit and contents, including the flooded weight during hydrostatic test.

For units with removable tube bundles, supports should be designed to withstand a pulling force equal to 1-1/2 times the weight of the tube bundle.

For purposes of support design, forces from external nozzle loadings, wind and seismic events are assumed to be negligible unless the purchaser specifically details the requirements. When these additional loads and forces are required to be considered, the combinations need not be assumed to occur simultaneously.

The references under Paragraph G-7.13 may be used for calculating resulting stresses due to the saddle supports.

Horizontal units are normally provided with at least two saddle type supports, with holes for anchor bolts. The holes in all but one of the supports are to be elongated to accommodate axial movement of the unit under operating conditions. Other types of support may be used if all design criteria are met, and axial movement is accommodated.

***G-7.12 VERTICAL UNITS**

Vertical units are to be provided with supports adequate to meet design requirements. The supports may be of the lug, annular ring, leg or skirt type. If the unit is to be located in a supporting structure, the supports should be of sufficient size to allow clearance for the body flanges.

SECTION 3 GENERAL FABRICATION AND PERFORMANCE INFORMATION

G-7.13 REFERENCES

- (1) Zick, L. P., "Stresses in Large Horizontal Cylindrical Pressure Vessels on Two Saddle Supports," Pressure Vessel and Piping; Design and Analysis, ASME, 1972.
- (2) Vinet, R., and Dore, R., "Stresses and Deformations in a Cylindrical Shell Lying on a Continuous Rigid Support," Paper No. 75-AM-1, Journal of Applied Mechanics, Trans. ASME.
- (3) Krupka, V., "An Analysis for Lug or Saddle Supported Cylindrical Pressure Vessels," Proceedings of the First International Conference on Pressure Vessel Technology, pp. 491-500.
- (4) Singh, K. P., Soler, A. I., "Mechanical Design of Heat Exchangers and Pressure Vessel Components," Chapter 17, Arcturus Publishers, Inc.
- (5) Bijlaard, P. P., "Stresses from Local Loadings in Cylindrical Pressure Vessels," Trans. ASME, Vol. 77, No. 6, (August 1955).
- (6) Wichman, K. R., Hopper, A. G., and Mershon, J. L., "Local Stresses in Spherical and Cylindrical Shells due to External Loadings," Welding Research Council, Bulletin No. 107, Rev. 1.
- (7) Rodabaugh, E. C., Dodge, W. G., and Moore, S. E., "Stress Indices at Lug Supports on Piping Systems," Welding Research Council Bulletin No. 198.
- (8) Brownell, L. E., and Young, E. H., "Process Equipment Design," John Wiley & Sons Inc.
- (9) Jawad, M. H., and Farr, J. R., "Structural Analysis and Design of Process Equipment," John Wiley and Sons, Inc., 1984.
- (10) Bednar, H. H., "Pressure Vessel Design Handbook," Van Nostrand Reinhold Company.
- (11) Blodgett, O. W., "Design of Welded Structures," The James F. Lincoln Arc Welding Foundation, 1966.
- (12) Moss, Dennis R., "Pressure Vessel Design Manual," 1987, Gulf Publishing Company.

*G-7.2 LIFTING DEVICES

Channels, bonnets, and covers which weigh over 60 lbs. (27.2 Kg) are to be provided with lifting lugs, rings or tapped holes for eyebolts. Unless otherwise specified, these lifting devices are designed to lift only the component to which they are directly attached.

Lugs for lifting the complete unit are not normally provided. When lifting lugs or trunnions are required by the purchaser to lift the complete unit, the device must be adequately designed.

- (1) The purchaser shall inform the manufacturer about the way in which the lifting device will be used. The purchaser shall be notified of any limitations of the lifting device relating to design or method of rigging.
- (2) Liquid penetrant examination of the lifting device attachment weld should be considered on large-heavy units.
- (3) The design load shall incorporate an appropriate impact factor.
- (4) Plate-type lifting lugs should be oriented to minimize bending stresses.
- (5) The hole diameter in the lifting device must be large enough to accept a shackle pin having a load rating greater than the design load.
- (6) The effect on the unit component to which the lifting device is attached should be considered. It may be necessary to add a reinforcing plate, annular ring or pad to distribute the load.
- (7) The adequacy of the exchanger to accommodate the lifting loads should be evaluated.

*G-7.3 WIND & SEISMIC DESIGN

For wind and seismic forces to be considered in the design of a heat exchanger, the purchaser must specify in the inquiry the design requirements. The "Recommended Good Practice" section of these Standards provides the designer with a discussion on this subject and selected references for design application.

E-1 PERFORMANCE OF HEAT EXCHANGERS

Satisfactory operation of heat exchangers can be obtained only from units which are properly designed and have built-in quality. Correct installation and preventive maintenance are user responsibilities.

E-1.1 PERFORMANCE FAILURES

The failure of heat exchanger equipment to perform satisfactorily may be caused by one or more factors, such as:

- (1) Excessive fouling.
- (2) Air or gas binding resulting from improper piping installation or lack of suitable vents.
- (3) Operating conditions differing from design conditions.
- (4) Maldistribution of flow in the unit.
- (5) Excessive clearances between the baffles and shell and/or tubes, due to corrosion.
- (6) Improper thermal design.

The user's best assurance of satisfactory performance lies in dependence upon manufacturers competent in the design and fabrication of heat transfer equipment.

E-2 INSTALLATION OF HEAT EXCHANGERS

E-2.1 HEAT EXCHANGER SETTINGS

E-2.11 CLEARANCE FOR DISMANTLING

For straight tube exchangers fitted with removable bundles, provide sufficient clearance at the stationary head end to permit removal of the bundle from the shell and provide adequate space beyond the rear head to permit removal of the shell cover and/or floating head cover.

For fixed tubesheet exchangers, provide sufficient clearance at one end to permit withdrawal and replacement of the tubes, and enough space beyond the head at the opposite end to permit removal of the bonnet or channel cover.

For U-tube heat exchangers, provide sufficient clearance at the stationary head end to permit withdrawal of the tube bundle, or at the opposite end to permit removal of the shell.

E-2.12 FOUNDATIONS

Foundations must be adequate so that exchangers will not settle and impose excessive strains on the exchanger. Foundation bolts should be set to allow for setting inaccuracies. In concrete footings, pipe sleeves at least one size larger than bolt diameter slipped over the bolt and cast in place are best for this purpose, as they allow the bolt center to be adjusted after the foundation has set.

E-2.13 FOUNDATION BOLTS

Foundation bolts should be loosened at one end of the unit to allow free expansion of shells. Slotted holes in supports are provided for this purpose.

E-2.14 LEVELING

Exchangers must be set level and square so that pipe connections may be made without forcing.

E-2.2 CLEANLINESS PROVISIONS

E-2.21 CONNECTION PROTECTORS

All exchanger openings should be inspected for foreign material. Protective plugs and covers should not be removed until just prior to installation.

E-2.22 DIRT REMOVAL

The entire system should be clean before starting operation. Under some conditions, the use of strainers in the piping may be required.

SECTION 4 INSTALLATION, OPERATION AND MAINTENANCE

E-2.23 CLEANING FACILITIES

Convenient means should be provided for cleaning the unit as suggested under "Maintenance of Heat Exchangers," Paragraph E-4.

E-2.3 FITTINGS AND PIPING

E-2.31 BY-PASS VALVES

It may be desirable for purchaser to provide valves and by-passes in the piping system to permit inspection and repairs.

E-2.32 TEST CONNECTIONS

When not integral with the exchanger nozzles, thermometer well and pressure gage connections should be installed close to the exchanger in the inlet and outlet piping.

E-2.33 VENTS

Vent valves should be provided by purchaser so units can be purged to prevent vapor or gas binding. Special consideration must be given to discharge of hazardous or toxic fluids.

E-2.34 DRAINS

Drains may discharge to atmosphere, if permissible, or into a vessel at lower pressure. They should not be piped to a common closed manifold.

E-2.35 PULSATION AND VIBRATION

In all installations, care should be taken to eliminate or minimize transmission of fluid pulsations and mechanical vibrations to the heat exchangers.

E-2.36 SAFETY RELIEF DEVICES

The ASME Code defines the requirements for safety relief devices. When specified by the purchaser, the manufacturer will provide the necessary connections for the safety relief devices. The size and type of the required connections will be specified by the purchaser. The purchaser will provide and install the required relief devices.

E-3 OPERATION OF HEAT EXCHANGERS

E-3.1 DESIGN AND OPERATING CONDITIONS

Equipment must not be operated at conditions which exceed those specified on the name plate(s).

E-3.2 OPERATING PROCEDURES

Before placing any exchanger in operation, reference should be made to the exchanger drawings, specification sheet(s) and name plate(s) for any special instructions. Local safety and health regulations must be considered. Improper start-up or shut-down sequences, particularly of fixed tubesheet units, may cause leaking of tube-to-tubesheet and/or bolted flanged joints.

E-3.21 START-UP OPERATION

Most exchangers with removable tube bundles may be placed in service by first establishing circulation of the cold medium, followed by the gradual introduction of the hot medium. During start-up all vent valves should be opened and left open until all passages have been purged of air and are completely filled with fluid. For fixed tubesheet exchangers, fluids must be introduced in a manner to minimize differential expansion between the shell and tubes.

E-3.22 SHUT-DOWN OPERATION

For exchangers with removable bundles, the units may be shut down by first gradually stopping the flow of the hot medium and then stopping the flow of the cold medium. If it is necessary to stop the flow of cold medium, the circulation of hot medium through the exchanger should also be stopped. For fixed tubesheet exchangers, the unit must be shut down in a manner to minimize differential expansion between shell and tubes. When shutting down the system, all units should be drained completely when there is the possibility of freezing or corrosion damage. To guard against water hammer, condensate should be

drained from steam heaters and similar apparatus during start-up or shut-down. To reduce water retention after drainage, the tube side of water cooled exchangers should be blown out with air.

E-3.23 TEMPERATURE SHOCKS

Exchangers normally should not be subjected to abrupt temperature fluctuations. Hot fluid must not be suddenly introduced when the unit is cold, nor cold fluid suddenly introduced when the unit is hot.

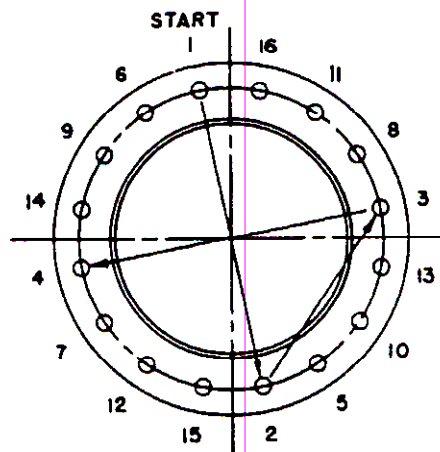
E-3.24 BOLTED JOINTS

Heat exchangers are pressure tested before leaving the manufacturer's shop in accordance with ASME Code requirements. However, normal relaxing of the gasketed joints may occur in the interval between testing in the manufacturer's shop and installation at the jobsite. Therefore, all external bolted joints may require retightening after installation and, if necessary, after the exchanger has reached operating temperature.

E-3.25 RECOMMENDED BOLT TIGHTENING PROCEDURE

It is important that all bolted joints be tightened uniformly and in a diametrically staggered pattern, as illustrated in Figure E-3.25, except for special high pressure closures when the instructions of the manufacturer should be followed.

FIGURE E-3.25



E-4 MAINTENANCE OF HEAT EXCHANGERS

E-4.1 INSPECTION OF UNIT

At regular intervals and as frequently as experience indicates, an examination should be made of the interior and exterior condition of the unit. Neglect in keeping all tubes clean may result in complete stoppage of flow through some tubes which could cause severe thermal strains, leaking tube joints, or structural damage to other components. Sacrificial anodes, when provided, should be inspected to determine whether they should be cleaned or replaced.

E-4.11 INDICATIONS OF FOULING

Exchangers subject to fouling or scaling should be cleaned periodically. A light sludge or scale coating on the tube greatly reduces its efficiency. A marked increase in pressure drop and/or reduction in performance usually indicates cleaning is necessary. The unit should first be checked for air or vapor binding to confirm that this is not the cause for the reduction in performance. Since the difficulty of cleaning increases rapidly as the scale thickness or deposit increases, the intervals between cleanings should not be excessive.

E-4.12 DISASSEMBLY FOR INSPECTION OR CLEANING

Before disassembly, the user must assure himself that the unit has been depressurized, vented and drained, neutralized and/or purged of hazardous material.

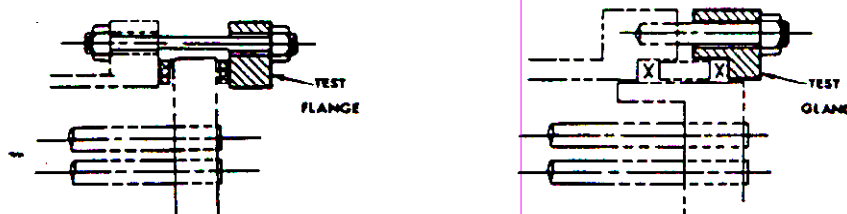
To inspect the inside of the tubes and also make them accessible for cleaning, the following procedures should be used:

- (1) Stationary Head End
 - (a) Type A, C, D & N, remove cover only
 - (b) Type B, remove bonnet
- (2) Rear Head End
 - (a) Type L, N & P, remove cover only
 - (b) Type M, remove bonnet
 - (c) Type S & T, remove shell cover and floating head cover
 - (d) Type W, remove channel cover or bonnet

E-4.13 LOCATING TUBE LEAKS

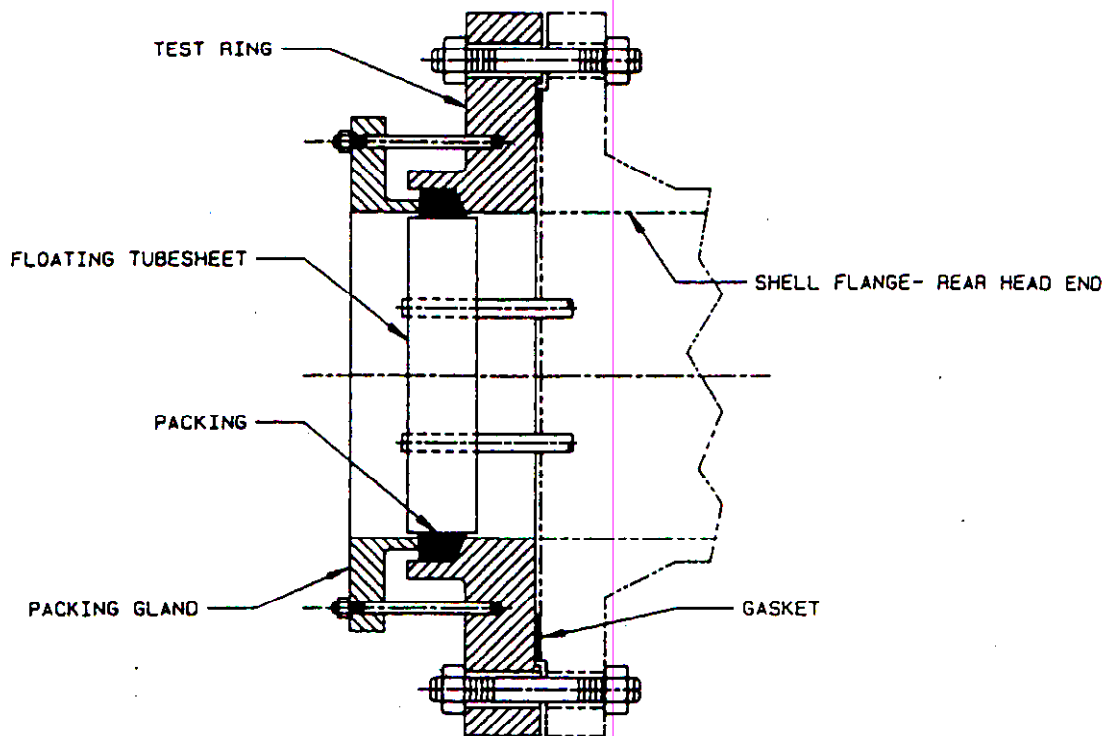
The following procedures may be used to locate perforated or split tubes and leaking joints between tubes and tubesheets. In most cases, the entire front face of each tubesheet will be accessible for inspection. The point where water escapes indicates a defective tube or tube-to-tubesheet joint.

- (1) Units with removable channel cover: Remove channel cover and apply hydraulic pressure in the shell.
- (2) Units with bonnet type head: For fixed tubesheet units where tubesheets are an integral part of the shell, remove bonnet and apply hydraulic pressure in the shell. For fixed tubesheet units where tubesheets are not an integral part of the shell and for units with removable bundles, remove bonnet, re-bolt tubesheet to shell or install test flange or gland, whichever is applicable, and apply hydraulic pressure in the shell. See Figure E-4.13-1 for typical test flange and test gland.

FIGURE E-4.13-1

- (3) Units with Type S or T floating head: Remove channel cover or bonnet, shell cover and floating head cover. Install test ring and bolt in place with gasket and packing. Apply hydraulic pressure in the shell. A typical test ring is shown in Figure E-4.13-2. When a test ring is not available it is possible to locate leaks in the floating head end by removing the shell cover and applying hydraulic pressure in the tubes. Leaking tube joints may then be located by sighting through the tube lanes. Care must be exercised when testing partially assembled exchangers to prevent over extension of expansion joints or overloading of tubes and/or tube-to-tubesheet joints.
- (4) Hydrostatic test should be performed so that the temperature of the metal is over 60° F (16° C) unless the materials of construction have a lower nil-ductility transition temperature.

FIGURE E-4.13-2



E-4.2 TUBE BUNDLE REMOVAL AND HANDLING

To avoid possible damage during removal of a tube bundle from a shell, a pulling device should be attached to eyebolts screwed into the tubesheet. If the tubesheet does not have tapped holes for eyebolts, steel rods or cables inserted through tubes and attached to bearing plates may be used. The bundle should be supported on the tube baffles, supports or tubesheets to prevent damage to the tubes.

Gasket and packing contact surfaces should be protected.

E-4.3 CLEANING TUBE BUNDLES

E-4.31 CLEANING METHODS

The heat transfer surfaces of heat exchangers should be kept reasonably clean to assure satisfactory performance. Convenient means for cleaning should be made available.

Heat exchangers may be cleaned by either chemical or mechanical methods. The method selected must be the choice of the operator of the plant and will depend on the type of deposit and the facilities available in the plant. Following are several cleaning procedures that may be considered:

- (1) Circulating hot wash oil or light distillate through tubes or shell at high velocity may effectively remove sludge or similar soft deposits.
- (2) Some salt deposits may be washed out by circulating hot fresh water.
- (3) Commercial cleaning compounds are available for removing sludge or scale provided hot wash oil or water is not available or does not give satisfactory results.
- (4) High pressure water jet cleaning.
- (5) Scrapers, rotating wire brushes, and other mechanical means for removing hard scale, coke, or other deposits.

- (6) Employ services of a qualified organization that provides cleaning services. These organizations will check the nature of the deposits to be removed, furnish proper solvents and/or acid solutions containing inhibitors, and provide equipment and personnel for a complete cleaning job.

E-4.32 CLEANING PRECAUTIONS

- (1) Tubes should not be cleaned by blowing steam through individual tubes since this heats the tube and may result in severe expansion strain, deformation of the tube, or loosening of the tube-to-tubesheet joint.
- (2) When mechanically cleaning a tube bundle, care should be exercised to avoid damaging the tubes.
- (3) Cleaning compounds must be compatible with the metallurgy of the exchanger.

E-4.4 TUBE EXPANDING

A suitable tube expander should be used to tighten a leaking tube joint. Care should be taken to ensure that tubes are not over expanded.

E-4.5 GASKET REPLACEMENT

Gaskets and gasket surfaces should be thoroughly cleaned and should be free of scratches and other defects. Gaskets should be properly positioned before attempting to retighten bolts. It is recommended that when a heat exchanger is dismantled for any cause, it be reassembled with new gaskets. This will tend to prevent future leaks and/or damage to the gasket seating surfaces of the heat exchanger. Composition gaskets become dried out and brittle so that they do not always provide an effective seal when reused. Metal or metal jacketed gaskets, when compressed initially, flow to match their contact surfaces. In so doing they are work hardened and, if reused, may provide an imperfect seal or result in deformation and damage to the gasket contact surfaces of the exchanger.

Bolted joints and flanges are designed for use with the particular type of gasket specified. Substitution of a gasket of different construction or improper dimensions may result in leakage and damage to gasket surfaces. Therefore, any gasket substitutions should be of compatible design.

Any leakage at a gasketed joint should be rectified and not permitted to persist as it may result in damage to the gasket surfaces.

Metal jacketed type gaskets are widely used. When these are used with a tongue and groove joint without a nubbin, the gasket should be installed so that the tongue bears on the seamless side of the gasket jacket. When a nubbin is used, the nubbin should bear on the seamless side.

E-4.6 SPARE AND REPLACEMENT PARTS

The procurement of spare or replacement parts from the manufacturer will be facilitated if the correct name for the part, as shown in Section 1, Table N-2, of these Standards is given, together with the serial number, type, size, and other information from the name plate. Replacement parts should be purchased from the original manufacturer.

E-4.7 PLUGGING OF TUBES

In U-tube heat exchangers, and other exchangers of special design, it may not be feasible to remove and replace defective tubes. Defective tubes may be plugged using commercially available tapered plugs with ferrules or tapered only plugs which may or may not be seal welded. Excessive tube plugging may result in reduced thermal performance, higher pressure drop, and/or mechanical damage. It is the user's responsibility to remove plugs and neutralize the bundle prior to sending it to a shop for repairs.

SECTION 5

MECHANICAL STANDARDS TEMA CLASS R C B

RCB-1 SCOPE AND GENERAL REQUIREMENTS

RCB-1.1 SCOPE OF STANDARDS

RCB-1.11 GENERAL

The TEMA Mechanical Standards are applicable to shell and tube heat exchangers which do not exceed any of the following criteria:

- (1) inside diameters of 100 inches (2540 mm)
- (2) product of nominal diameter, inches (mm) and design pressure, psi (kPa) of 100,000 (17.5×10^6)
- (3) a design pressure of 3,000 psi (20684 kPa)

The intent of these parameters is to limit the maximum shell wall thickness to approximately 3 inches (76 mm), and the maximum stud diameter to approximately 4 inches (102 mm). Criteria contained in these Standards may be applied to units which exceed the above parameters.

R-1.12 DEFINITION OF TEMA CLASS "R" EXCHANGERS

The TEMA Mechanical Standards for Class "R" heat exchangers specify design and fabrication of unfired shell and tube heat exchangers for the generally severe requirements of petroleum and related processing applications.

C-1.12 DEFINITION OF TEMA CLASS "C" EXCHANGERS

The TEMA Mechanical Standards for Class "C" heat exchangers specify design and fabrication of unfired shell and tube heat exchangers for the generally moderate requirements of commercial and general process applications.

B-1.12 DEFINITION OF TEMA CLASS "B" EXCHANGERS

The TEMA Mechanical Standards for Class "B" heat exchangers specify design and fabrication of unfired shell and tube heat exchangers for chemical process service.

RCB-1.13 CONSTRUCTION CODES

The individual vessels shall comply with the ASME (American Society of Mechanical Engineers) Boiler and Pressure Vessel Code, Section VIII, Division 1, hereinafter referred to as the Code. These Standards supplement and define the Code for heat exchanger applications. The manufacturer shall comply with the construction requirements of state and local codes when the purchaser specifies the plant location. It shall be the responsibility of the purchaser to inform the manufacturer of any applicable local codes. Application of the Code symbol is required, unless otherwise specified by the purchaser.

RCB-1.14 MATERIALS-DEFINITION OF TERMS

For purposes of these Standards, "carbon steel" shall be construed as any steel or low alloy falling within the scope of Part UCS of the Code. Metals not included by the foregoing (except cast iron) shall be considered as "alloys" unless otherwise specifically named. Materials of construction, including gaskets, should be specified by the purchaser. The manufacturer assumes no responsibility for deterioration of parts for any reason.

RCB-1.2 DESIGN PRESSURE

RCB-1.21 DESIGN PRESSURE

Design pressures for the shell and tube sides shall be specified separately by the purchaser.

RCB-1.3 TESTING

RCB-1.31 STANDARD TEST

The exchanger shall be hydrostatically tested with water. The test pressure shall be held for at least 30 minutes. The shell side and the tube side are to be tested separately in such a manner that leaks at the tube joints can be detected from at least one side. When the tube side design pressure is the higher pressure, the tube bundle shall be tested outside of the shell only if specified by the purchaser and the construction permits. Welded joints are to be

sufficiently cleaned prior to testing the exchanger to permit proper inspection during the test. The minimum hydrostatic test pressure at room temperature shall be in accordance with the Code.

RCB-1.311 OTHER LIQUID TESTS

Liquids other than water may be used as a testing medium if agreed upon between the purchaser and the manufacturer.

RCB-1.32 PNEUMATIC TEST

When liquid cannot be tolerated as a test medium the exchanger may be given a pneumatic test in accordance with the Code. It must be recognized that air or gas is hazardous when used as a pressure testing medium. The pneumatic test pressure at room temperature shall be in accordance with the Code.

RCB-1.33 SUPPLEMENTARY AIR TEST

When a supplementary air or gas test is specified by the purchaser, it shall be preceded by the hydrostatic test required by Paragraph RCB-1.31. The test pressure shall be as agreed upon by the purchaser and manufacturer, but shall not exceed that required by Paragraph RCB-1.32.

RCB-1.4 METAL TEMPERATURES**RCB-1.41 METAL TEMPERATURE LIMITATIONS FOR PRESSURE PARTS**

The metal temperature limitations for various metals are those prescribed by the Code.

RCB-1.42 DESIGN TEMPERATURE OF HEAT EXCHANGER PARTS**RCB-1.421 FOR PARTS NOT IN CONTACT WITH BOTH FLUIDS**

Design temperatures for the shell and tube sides shall be specified separately by the purchaser. The Code provides the allowable stress limits for parts to be designed at the specified design temperature.

RCB-1.422 FOR PARTS IN CONTACT WITH BOTH FLUIDS

The design temperature is the design metal temperature and is used to establish the Code stress limits for design. The design metal temperature shall be based on the operating temperatures of the shellside and the tubeside fluids, except when the purchaser specifies some other design metal temperature. When the design metal temperature is less than the higher of the design temperatures referred to in Paragraph RCB-1.421, the design metal temperature and the affected parts shall be shown on the manufacturer's nameplate(s) as described in Paragraph G-3.1.

RCB-1.43 MEAN METAL TEMPERATURES**RCB-1.431 FOR PARTS NOT IN CONTACT WITH BOTH FLUIDS**

The mean metal temperature is the calculated metal temperature, under specified operating conditions, of a part in contact with a fluid. It is used to establish metal properties under operating conditions. The mean metal temperature is based on the specified operating temperatures of the fluid in contact with the part.

RCB-1.432 FOR PARTS IN CONTACT WITH BOTH FLUIDS

The mean metal temperature is the calculated metal temperature, under specified operating conditions, of a part in contact with both shellside and tubeside fluids. It is used to establish metal properties under operating conditions. The mean metal temperature is based on the specified operating temperatures of the shellside and tubeside fluids. In establishing the mean metal temperatures, due consideration shall be given to such factors as the relative heat transfer coefficients of the two fluids contacting the part and the relative heat transfer area of the parts contacted by the two fluids.

RCB-1.5 STANDARD CORROSION ALLOWANCES

The standard corrosion allowances used for the various heat exchanger parts are as follows, unless the conditions of service make a different allowance more suitable and such allowance is specified by the purchaser.

RCB-1.51 CARBON STEEL PARTS**R-1.511 PRESSURE PARTS**

All carbon steel pressure parts, except as noted below, are to have a corrosion allowance of 1/8" (3.2 mm).

CB-1.511 PRESSURE PARTS

All carbon steel pressure parts, except as noted below, are to have a corrosion allowance of 1/16" (1.6 mm).

RCB-1.512 INTERNAL FLOATING HEAD COVERS

Internal floating head covers are to have the corrosion allowance on all wetted surfaces except gasket seating surfaces. Corrosion allowance on the outside of the flanged portion may be included in the recommended minimum edge distance.

RCB-1.513 TUBESHEETS

Tubesheets are to have the corrosion allowance on each side with the provision that, on the grooved side of a grooved tubesheet, the depth of the gasketed groove may be considered as available for corrosion allowance.

RCB-1.514 EXTERNAL COVERS

Where flat external covers are grooved, the depth of the gasketed groove may be considered as available for corrosion allowance.

RCB-1.515 END FLANGES

Corrosion allowance shall be applied only to the inside diameter of flanges where exposed to the fluids.

RCB-1.516 NONPRESSURE PARTS

Nonpressure parts such as tie-rods, spacers, baffles and support plates are not required to have corrosion allowance.

RCB-1.517 TUBES, BOLTING AND FLOATING HEAD BACKING DEVICES

Tubes, bolting and floating head backing devices are not required to have corrosion allowance.

RCB-1.518 PASS PARTITION PLATES

Pass partition plates are not required to have corrosion allowance.

RCB-1.52 ALLOY PARTS

Alloy parts are not required to have corrosion allowance.

R-1.53 CAST IRON PARTS

Cast iron pressure parts shall have a corrosion allowance of 1/8" (3.2 mm).

CB-1.53 CAST IRON PARTS

Cast iron pressure parts shall have a corrosion allowance of 1/16" (1.6 mm).

RCB-1.6 SERVICE LIMITATIONS**RB-1.61 CAST IRON PARTS**

Cast iron shall be used only for water service at pressures not exceeding 150 psi (1034 kPa).

C-1.61 CAST IRON PARTS

Cast iron shall not be used for pressures exceeding 150 psi (1034 kPa), or for lethal or flammable fluids at any pressure.

RCB-1.62 EXTERNAL PACKED JOINTS

Packed joints shall not be used when the purchaser specifies that the fluid in contact with the joint is lethal or flammable.

RCB-1.7 ANODES

Selection and placement of anodes is not the responsibility of the heat exchanger manufacturer. If a heat exchanger is to be furnished with anodes, when requesting a quotation, the purchaser is responsible for furnishing the heat exchanger manufacturer the following information:

- (1) Method of anode attachment.
- (2) Quantity of anodes required.
- (3) Size and manufacturer of the anodes.
- (4) Anode material.
- (5) Sketch of anode locations and spacing.

If the heat exchanger manufacturer chooses to install anodes for a customer, the manufacturer is not responsible for the suitability of the anodes for the service it is installed in, the life of the anodes, the corrosion protection provided by the anode, or any subsequent damage to the heat exchanger attributed to the anode, the method of anode installation, or the installed location of the anode in the heat exchanger.

RCB-2 TUBES*RCB-2.1 TUBE LENGTH**

The following tube lengths for both straight and U-tube exchangers are commonly used: 96 (2438), 120 (3048), 144 (3658), 192 (4877) and 240 (6096) inches (mm). Other lengths may be used. Also see Paragraph N-1.12.

RCB-2.2 TUBE DIAMETERS AND GAGES**RCB-2.21 BARE TUBES**

Table RCB-2.21 lists common tube diameters and gages for bare tubes of copper, steel and alloy. Other diameters and gages are acceptable.

TABLE RCB-2.21

BARE TUBE DIAMETERS AND GAGES			
O.D. Inches (mm)	Copper and Copper Alloys	Carbon Steel, Aluminum and Aluminum Alloys	Other Alloys
	B.W.G.	B.W.G.	B.W.G.
1/4 (6.4)	27 24 22	- - -	27 24 22
3/8 (9.5)	22 20 18	- - -	22 20 18
1/2 (12.7)	20 18	- -	20 18
5/8 (15.9)	20 18 16	18 16 14	20 18 16
3/4 (19.1)	20 18 16	16 14 12	18 16 14
7/8 (22.2)	18 16 14 12	14 12 10 -	16 14 12 -
1 (25.4)	18 16 14	14 12 -	16 14 12
1-1/4 (31.8)	16 14	14 12	14 12
1-1/2 (38.1)	16 14	14 12	14 12
2 (50.8)	14 12	14 12	14 12

Notes:

1. Wall thickness shall be specified as either minimum or average.
2. Characteristics of tubing are shown in Tables D-7 and D7M.

RCB-2.22 INTEGRALLY FINNED TUBES

The nominal fin diameter shall not exceed the outside diameter of the unfinned section. Specified wall shall be based on the thickness at the root diameter.

RCB-2.3 U-TUBES

RCB-2.31 U-BEND REQUIREMENTS

When U-bends are formed, it is normal for the tube wall at the outer radius to thin. The minimum tube wall thickness in the bent portion before bending shall be:

$$t_0 = t_1 \left[1 + \frac{d_o}{4R} \right]$$

where

- t_0 = Original tube wall thickness, inches (mm)
- t_1 = Minimum tube wall thickness calculated by Code rules for a straight tube subjected to the same pressure and metal temperature, inches (mm)
- d_o = Outside tube diameter, inches (mm)
- R = Mean radius of bend, inches (mm)

More than one tube gage, or dual gage tubes, may be used in a tube bundle.

When U-bends are formed from tube materials which are relatively non-work-hardening and of suitable temper, tube wall thinning in the bends should not exceed a nominal 17% of original tube wall thickness.

Flattening at the bend shall not exceed 10% of the nominal tube outside diameter.

U-bends formed from tube materials having low ductility, or materials which are susceptible to work-hardening, may require special consideration. Also refer to Paragraph RCB-2.33.

RCB-2.32 BEND SPACING

RCB-2.321 CENTER-TO-CENTER DIMENSION

The center-to-center dimensions between parallel legs of U-tubes shall be such that they can be inserted into the baffle assembly without damage to the tubes.

RCB-2.322 BEND INTERFERENCE

The assembly of bends shall be of workmanlike appearance. Metal-to-metal contact between bends in the same plane shall not be permitted.

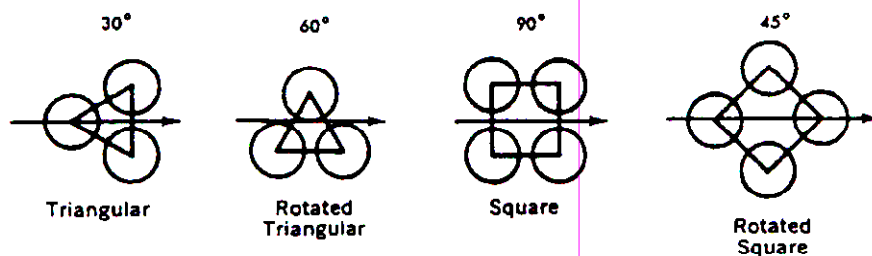
RCB-2.33 HEAT TREATMENT

Cold work in forming U-bends may induce embrittlement or susceptibility to stress corrosion in certain materials and/or environments. Heat treatment to alleviate such conditions may be performed by agreement between manufacturer and purchaser.

RCB-2.4 TUBE PATTERN

Standard tube patterns are shown in Figure RCB-2.4.

FIGURE RCB-2.4



Note: Flow arrows are perpendicular to the baffle cut edge.

RCB-2.41 SQUARE PATTERN

In removable bundle units, when mechanical cleaning of the tubes is specified by the purchaser, tube lanes should be continuous.

RCB-2.42 TRIANGULAR PATTERN

Triangular or rotated triangular pattern should not be used when the shell side is to be cleaned mechanically.

R-2.5 TUBE PITCH

Tubes shall be spaced with a minimum center-to-center distance of 1.25 times the outside diameter of the tube. When mechanical cleaning of the tubes is specified by the purchaser, minimum cleaning lanes of 1/4" (6.4 mm) shall be provided.

C-2.5 TUBE PITCH

Tubes shall be spaced with a minimum center-to-center distance of 1.25 times the outside diameter of the tube. Where the tube diameters are 5/8" (15.9 mm) or less and tube-to-tubesheet joints are expanded only, the minimum center-to-center distance may be reduced to 1.20 times the outside diameter.

B-2.5 TUBE PITCH

Tubes shall be spaced with a minimum center-to-center distance of 1.25 times the outside diameter of the tube. When mechanical cleaning of the tubes is specified by the purchaser and the nominal shell diameter is 12 inches (305 mm) or less, minimum cleaning lanes of 3/16" (4.8 mm) shall be provided. For shell diameters greater than 12 inches (305 mm), minimum cleaning lanes of 1/4" (6.4 mm) shall be provided.

SECTION 5

MECHANICAL STANDARDS TEMA CLASS R C B

RCB-3 SHELLS AND SHELL COVERS

RCB-3.1 SHELLS

RCB-3.11 SHELL DIAMETERS

It shall be left to the discretion of each manufacturer to establish a system of standard shell diameters within the TEMA Mechanical Standards in order to achieve the economies peculiar to his individual design and manufacturing facilities.

RCB-3.12 TOLERANCES

RCB-3.121 PIPE SHELLS

The inside diameter of pipe shells shall be in accordance with applicable ASTM/ASME pipe specifications.

RCB-3.122 PLATE SHELLS

The inside diameter of any plate shell shall not exceed the design inside diameter by more than 1/8" (3.2 mm) as determined by circumferential measurement.

RCB-3.13 MINIMUM SHELL THICKNESS

Shell thickness is determined by the Code design formulas, plus corrosion allowance, but in no case shall the nominal thickness of shells be less than that shown in the applicable table. The nominal total thickness for clad shells shall be the same as for carbon steel shells.

TABLE R-3.13
MINIMUM SHELL THICKNESS
Dimensions In Inches (mm)

Nominal Shell Diameter		Minimum Thickness				
		Carbon Steel		Alloy *		
		Pipe	Plate			
6	(152)	SCH. 40	-	-	1/8	(3.2)
8 - 12	(203-305)	SCH. 30	-	-	1/8	(3.2)
13 - 29	(330-737)	SCH. STD	3/8	(9.5)	3/16	(4.8)
30 - 39	(762-991)	-	7/16	(11.1)	1/4	(6.4)
40 - 60	(1016-1524)	-	1/2	(12.7)	5/16	(7.9)
61 - 80	(1549-2032)	-	1/2	(12.7)	5/16	(7.9)
81 - 100	(2057-2540)	-	1/2	(12.7)	3/8	(9.5)

TABLE CB-3.13
MINIMUM SHELL THICKNESS
Dimensions In Inches (mm)

Nominal Shell Diameter		Minimum Thickness				
		Carbon Steel		Alloy *		
		Pipe	Plate			
6	(152)	SCH. 40		-	1/8	(3.2)
8 - 12	(203-305)	SCH. 30		-	1/8	(3.2)
13 - 23	(330-584)	SCH. 20	5/16	(7.9)	1/8	(3.2)
24 - 29	(610-737)	-	5/16	(7.9)	3/16	(4.8)
30 - 39	(762-991)	-	3/8	(9.5)	1/4	(6.4)
40 - 60	(1016-1524)	-	7/16	(11.1)	1/4	(6.4)
61 - 80	(1549-2032)	-	1/2	(12.7)	5/16	(7.9)
81 - 100	(2057-2540)	-	1/2	(12.7)	3/8	(9.5)

*Schedule 5S is permissible for 6 inch (152 mm) and 8 inch (203 mm) shell diameters.

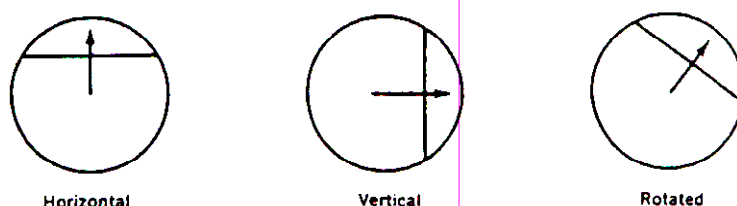
RCB-3.2 SHELL COVER THICKNESS

Nominal thickness of shell cover heads, before forming, shall be at least equal to the thickness of the shell as shown in the applicable table.

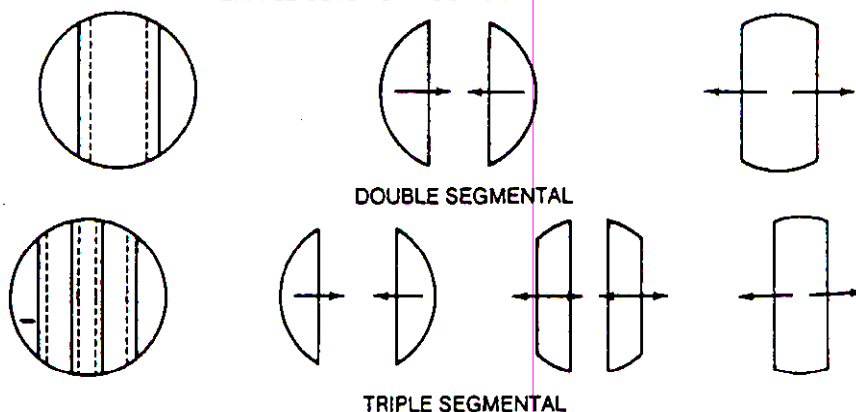
RCB-4 BAFFLES AND SUPPORT PLATES**RCB-4.1 TYPE OF TRANSVERSE BAFFLES**

The segmental or multi-segmental type of baffle or tube support plate is standard. Other type baffles are permissible. Baffle cut is defined as the segment opening height expressed as a percentage of the shell inside diameter or as a percentage of the total net free area inside the shell (shell cross sectional area minus total tube area). The number of tube rows that overlap for multi-segmental baffles should be adjusted to give approximately the same net free area flow through each baffle. Baffles shall be cut near the centerline of a row of tubes, of a pass lane, of a tube lane, or outside the tube pattern. Baffles shall have a workmanlike finish on the outside diameter. Typical baffle cuts are illustrated in Figure RCB-4.1. Baffle cuts may be vertical, horizontal or rotated.

FIGURE RCB-4.1
BAFFLE CUTS FOR SEGMENTAL BAFFLES



BAFFLE CUTS FOR MULTI-SEGMENTAL BAFFLES

**RCB-4.2 TUBE HOLES**

Where the maximum unsupported tube length is 36 inches (914 mm) or less, or for tubes larger in diameter than 1 1/4 inches (31.8 mm) OD, standard tube holes are to be 1/32 inch (0.8 mm) over the OD of the tubes. Where the unsupported tube length exceeds 36 inches (914 mm) for tubes 1 1/4 inches (31.8 mm) diameter and smaller, standard tube holes are to be 1/64 inch (0.4 mm) over the OD of the tubes. For pulsating conditions, tube holes may be smaller than standard. Any burrs shall be removed and the tube holes given a workmanlike finish. Baffle holes will have an over-tolerance of 0.010 inch (0.3 mm) except that 4% of the holes are allowed an over-tolerance of 0.015 inch (0.4 mm).

RCB-4.3 TRANSVERSE BAFFLE AND SUPPORT CLEARANCE

The transverse baffle and support plate clearance shall be such that the difference between the shell design inside diameter and the outside diameter of the baffle shall not exceed that indicated in Table RCB-4.3. However, where such clearance has no significant effect on shell side heat transfer coefficient or mean temperature difference, these maximum clearances may be increased to twice the tabulated values. (See Paragraph RCB-4.43.)

TABLE RCB-4.3

Standard Cross Baffle and Support Plate Clearances
Dimensions In Inches (mm)

Nominal Shell ID	Design ID of Shell Minus Baffle OD
6 - 17 (152-432)	1/8 (3.2)
18 - 39 (457-991)	3/16 (4.8)
40 - 54 (1016-1372)	1/4 (6.4)
55 - 69 (1397-1753)	5/16 (7.9)
70 - 84 (1778-2134)	3/8 (9.5)
85 - 100 (2159-2540)	7/16 (11.1)

The design inside diameter of a pipe shell is defined as the nominal outside diameter of the pipe, minus twice the nominal wall thickness. The design inside diameter of a plate shell is the specified inside diameter. In any case, the design inside diameter may be taken as the actual measured shell inside diameter.

RCB-4.4 THICKNESS OF BAFFLES AND SUPPORT PLATES

RCB-4.41 TRANSVERSE BAFFLES AND SUPPORT PLATES

The following tables show the minimum thickness of transverse baffles and support plates applying to all materials for various shell diameters and plate spacings.

The thickness of the baffle or support plates for U-tube bundles shall be based on the unsupported tube length in the straight section of the bundle. The U-bend length shall not be considered in determining the unsupported tube length for required plate thickness.

TABLE R-4.41

BAFFLE OR SUPPORT PLATE THICKNESS
Dimensions in Inches (mm)

Nominal Shell ID	Plate Thickness				
	Unsupported tube length between central baffles. End spaces between tubesheets and baffles are not a consideration.				
	24 (610) and Under	Over 24 (610) to 36 (914) Inclusive	Over 36 (914) to 48 (1219) Inclusive	Over 48 (1219) to 60 (1524) Inclusive	Over 60 (1524)
6 - 14 (152-356)	1/8 (3.2)	3/16 (4.8)	1/4 (6.4)	3/8 (9.5)	3/8 (9.5)
15 - 28 (381-711)	3/16 (4.8)	1/4 (6.4)	3/8 (9.5)	3/8 (9.5)	1/2 (12.7)
29 - 38 (737-965)	1/4 (6.4)	5/16 (7.5)	3/8 (9.5)	1/2 (12.7)	5/8 (15.9)
39 - 60 (991-1524)	1/4 (6.4)	3/8 (9.5)	1/2 (12.7)	5/8 (15.9)	5/8 (15.9)
61 - 100 (1549-2540)	3/8 (9.5)	1/2 (12.7)	5/8 (15.9)	3/4 (19.1)	3/4 (19.1)

TABLE CB-4.41
BAFFLE OR SUPPORT PLATE THICKNESS
 Dimensions in Inches (mm)

Nominal Shell ID	Plate Thickness					
	Unsupported tube length between central baffles. End spaces between tubesheets and baffles are not a consideration.					
	12 (305) and Under	Over 12 (305) to 24 (610) Inclusive	Over 24 (610) to 36 (914) Inclusive	Over 36 (914) to 48 (1219) Inclusive	Over 48 (1219) to 60 (1524) Inclusive	Over 60 (1524)
6 - 14 (152-356)	1/16 (1.6)	1/8 (3.2)	3/16 (4.8)	1/4 (6.4)	3/8 (9.5)	3/8 (9.5)
15 - 28 (381-711)	1/8 (3.2)	3/16 (4.8)	1/4 (6.4)	3/8 (9.5)	3/8 (9.5)	1/2 (12.7)
29 - 38 (737-965)	3/16 (4.8)	1/4 (6.4)	5/16 (7.5)	3/8 (9.5)	1/2 (12.7)	5/8 (15.9)
39 - 60 (991-1524)	1/4 (6.4)	1/4 (6.4)	3/8 (9.5)	1/2 (12.7)	5/8 (15.9)	5/8 (15.9)
61 - 100 (1549-2540)	1/4 (6.4)	3/8 (9.5)	1/2 (12.7)	5/8 (15.9)	3/4 (19.1)	3/4 (19.1)

R-4.42 LONGITUDINAL BAFFLES

Longitudinal baffles shall not be less than 1/4" (6.4 mm) nominal metal thickness.

CB-4.42 LONGITUDINAL BAFFLES

Longitudinal carbon steel baffles shall not be less than 1/4" (6.4 mm) nominal metal thickness.

Longitudinal alloy baffles shall not be less than 1/8" (3.2 mm) nominal metal thickness.

RCB-4.43 SPECIAL PRECAUTIONS

Special consideration should be given to:

- (1) Baffles and support plates subjected to pulsations.
- (2) Baffles and support plates engaging finned tubes.
- (3) Longitudinal baffles subjected to large differential pressures due to high shell side fluid pressure drop.
- (4) Support of tube bundles when larger clearances allowed by RCB-4.3 are used.

RCB-4.5 SPACING OF BAFFLES AND SUPPORT PLATES**RCB-4.51 MINIMUM SPACING**

Segmental baffles normally should not be spaced closer than 1/5 of the shell ID or 2 inches (51 mm), whichever is greater. However, special design considerations may dictate a closer spacing.

RCB-4.52 MAXIMUM SPACING

Tube support plates shall be so spaced that the unsupported tube span does not exceed the value indicated in Table RCB-4.52 for the tube material used.

TABLE RCB-4.52
MAXIMUM UNSUPPORTED STRAIGHT TUBE SPANS
 Dimensions in Inches (mm)

Tube OD	Tube Materials and Temperature Limits ° F (° C)	
	Carbon Steel & High Alloy Steel, 750 (399) Low Alloy Steel, 850 (454) Nickel-Copper, 600 (316) Nickel, 850 (454) Nickel-Chromium-Iron, 1000 (538)	Aluminum & Aluminum Alloys, Copper & Copper Alloys, Titanium Alloys At Code Maximum Allowable Temperature
1/4 (6.4)	26 (660)	22 (559)
3/8 (9.5)	35 (889)	30 (762)
1/2 (12.7)	44 (1118)	38 (965)
5/8 (15.9)	52 (1321)	45 (1143)
3/4 (19.1)	60 (1524)	52 (1321)
7/8 (22.2)	69 (1753)	60 (1524)
1 (25.4)	74 (1880)	64 (1626)
1-1/4 (31.8)	88 (2235)	76 (1930)
1-1/2 (38.1)	100 (2540)	87 (2210)
2 (50.8)	125 (3175)	110 (2794)

Notes:

- (1) Above the metal temperature limits shown, maximum spans shall be reduced in direct proportion to the fourth root of the ratio of elastic modulus at temperature to elastic modulus at tabulated limit temperature.
- (2) In the case of circumferentially finned tubes, the tube OD shall be the diameter at the root of the fins and the corresponding tabulated or interpolated span shall be reduced in direct proportion to the fourth root of the ratio of the weight per unit length of the tube, if stripped of fins to that of the actual finned tube.
- (3) The maximum unsupported tube spans in Table RCB-4.52 do not consider potential flow induced vibration problems. Refer to Section 6 for vibration criteria.

RCB-4.53 BAFFLE SPACING

Baffles normally shall be spaced uniformly, spanning the effective tube length. When this is not possible, the baffles nearest the ends of the shell, and/or tubesheets, shall be located as close as practical to the shell nozzles. The remaining baffles normally shall be spaced uniformly.

RCB-4.54 U-TUBE REAR SUPPORT

The support plates or baffles adjacent to the bends in U-tube exchangers shall be so located that, for any individual bend, the sum of the bend diameter plus the straight lengths measured along both legs from supports to bend tangents does not exceed the maximum unsupported span determined from Paragraph RCB-4.52. Where bend diameters prevent compliance, special provisions in addition to the above shall be made for support of the bends.

RCB-4.55 SPECIAL CASES

When pulsating conditions are specified by the purchaser, unsupported spans shall be as short as pressure drop restrictions permit. If the span under these circumstances approaches the maximum permitted by Paragraph RCB-4.52, consideration should be given to alternative flow arrangements which would permit shorter spans under the same pressure drop restrictions.

RCB-4.56 TUBE BUNDLE VIBRATION

Shell side flow may produce excitation forces which result in destructive tube vibrations. Existing predictive correlations are inadequate to insure that any given design will be free of such damage. The vulnerability of an exchanger to flow induced vibration depends on the flow rate, tube and baffle materials, unsupported tube spans, tube field layout, shell diameter, and inlet/outlet configuration. Section 6 of these Standards contains information which is

intended to alert the designer to potential vibration problems. In any case, and consistent with Paragraph G-5, the manufacturer is not responsible or liable for any direct, indirect, or consequential damages resulting from vibration.

RCB-4.6 IMPINGEMENT BAFFLES AND EROSION PROTECTION

The following paragraphs provide limitations to prevent or minimize erosion of tube bundle components at the entrance and exit areas. These limitations have no correlation to tube vibration and the designer should refer to Section 6 for information regarding this phenomenon.

RCB-4.61 SHELL SIDE IMPINGEMENT PROTECTION REQUIREMENTS

An impingement plate, or other means to protect the tube bundle against impinging fluids, shall be provided when entrance line values of ρV^2 exceed the following: non-abrasive, single phase fluids, 1500 (2232); all other liquids, including a liquid at its boiling point, 500 (744). For all other gases and vapors, including all nominally saturated vapors, and for liquid vapor mixtures, impingement protection is required. V is the linear velocity of the fluid in feet per second (meters per second) and ρ is its density in pounds per cubic foot (kilograms per cubic meter). A properly designed diffuser may be used to reduce line velocities at shell entrance.

*RCB-4.62 SHELL OR BUNDLE ENTRANCE AND EXIT AREAS

In no case shall the shell or bundle entrance or exit area produce a value of ρV^2 in excess of 4,000 (5953) where V is the linear velocity of the fluid in feet per second (meters per second) and ρ is its density in pounds per cubic foot (kilograms per cubic meter).

*RCB-4.621 SHELL ENTRANCE OR EXIT AREA WITH IMPINGEMENT PLATE

When an impingement plate is provided, the flow area shall be considered the unrestricted area between the inside diameter of the shell at the nozzle and the face of the impingement plate.

*RCB-4.622 SHELL ENTRANCE OR EXIT AREA WITHOUT IMPINGEMENT PLATE

For determining the area available for flow at the entrance or exit of the shell where there is no impingement plate, the flow area between the tubes within the projection of the nozzle bore and the actual unrestricted radial flow area from under the nozzle or dome measured between the tube bundle and shell inside diameter may be considered.

*RCB-4.623 BUNDLE ENTRANCE OR EXIT AREA WITH IMPINGEMENT PLATE

When an impingement plate is provided under a nozzle, the flow area shall be the unrestricted area between the tubes within the compartments between baffles and/or tubesheet.

*RCB-4.624 BUNDLE ENTRANCE OR EXIT AREA WITHOUT IMPINGEMENT PLATE

For determining the area available for flow at the entrance or exit of the tube bundle where there is no impingement plate, the flow area between the tubes within the compartments between baffles and/or tubesheet may be considered.

RCB-4.63 TUBE SIDE

Consideration shall be given to the need for special devices to prevent erosion of the tube ends under the following conditions:

- (1) Use of an axial inlet nozzle.
- (2) Liquid ρV^2 is in excess of 6000 (8928), where V is the linear velocity in feet per second (meter per second), and ρ is its density in pounds per cubic foot (kilograms per cubic meter).

RCB-4.7 TIE RODS AND SPACERS

Tie rods and spacers, or other equivalent means of tying the baffle system together, shall be provided to retain all transverse baffles and tube support plates securely in position.

R-4.71 NUMBER AND SIZE OF TIE RODS

Table R-4.71 shows suggested tie rod count and diameter for various sizes of heat exchangers. Other combinations of tie rod number and diameter with equivalent metal area are permissible; however, no fewer than four tie rods, and no diameter less than 3/8" (9.5 mm) shall be used. Any baffle segment requires a minimum of three points of support.

TABLE R-4.71
TIE ROD STANDARDS
Dimensions in Inches (mm)

Nominal Shell Diameter	Tie Rod Diameter	Minimum Number of Tie Rods
6 - 15 (152-381)	3/8 (9.5)	4
16 - 27 (406-686)	3/8 (9.5)	6
28 - 33 (711-838)	1/2 (12.7)	6
34 - 48 (864-1219)	1/2 (12.7)	8
49 - 60 (1245-1524)	1/2 (12.7)	10
61-100 (1549-2540)	5/8 (15.9)	12

CB-4.71 NUMBER AND SIZE OF TIE RODS

Table CB-4.71 shows suggested tie rod count and diameter for various sizes of heat exchangers. Other combinations of tie rod number and diameter with equivalent metal area are permissible; however, no fewer than four tie rods, and no diameter less than 3/8" (9.5 mm) shall be used above 15 inch (381) nominal shell diameter. Any baffle segment requires a minimum of three points of support.

TABLE CB-4.71
TIE ROD STANDARDS
Dimensions in Inches (mm)

Nominal Shell Diameter	Tie Rod Diameter	Minimum Number of Tie Rods
6 - 15 (152-381)	1/4 (6.4)	4
16 - 27 (406-686)	3/8 (9.5)	6
28 - 33 (711-838)	1/2 (12.7)	6
34 - 48 (864-1219)	1/2 (12.7)	8
49 - 60 (1245-1524)	1/2 (12.7)	10
61-100 (1549-2540)	5/8 (15.9)	12

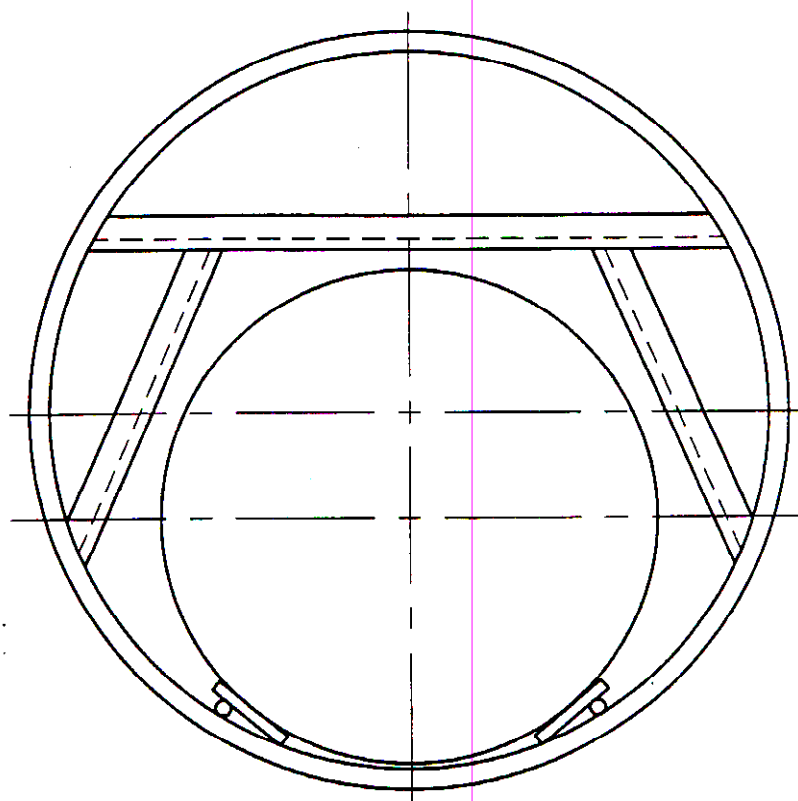
RCB-4.8 SEALING DEVICES

In addition to the baffles, sealing devices should be installed when necessary to prevent excessive fluid by-passing around or through the tube bundle. Sealing devices may be seal strips, tie rods with spacers, dummy tubes, or combinations of these.

RCB-4.9 KETTLE TYPE REBOILERS

For kettle type reboilers, skid bars and a bundle hold-down may be provided. One method is shown in Figure RCB-4.9. Other methods which satisfy the intent are acceptable. Bundle hold-downs are not required for fixed tubesheet kettles.

FIGURE RCB-4.9



CROSS-SECTION END VIEW OF TUBE BUNDLE AND SHELL

RCB-5 FLOATING END CONSTRUCTION

RCB-5.1 INTERNAL FLOATING HEADS (Types S and T)

R-5.11 MINIMUM INSIDE DEPTH OF FLOATING HEAD COVERS

For multipass floating head covers the inside depth shall be such that the minimum cross-over area for flow between successive tube passes is at least equal to 1.3 times the flow area through the tubes of one pass. For single pass floating head covers the depth at nozzle centerline shall be a minimum of one-third the inside diameter of the nozzle.

CB-5.11 MINIMUM INSIDE DEPTH OF FLOATING HEAD COVERS

For multipass floating head covers the inside depth shall be such that the minimum cross-over area for flow between successive tube passes is at least equal to the flow area through the tubes of one pass. For single pass floating head covers the depth at nozzle centerline shall be a minimum of one-third the inside diameter of the nozzle.

RCB-5.12 POSTWELD HEAT TREATMENT

Fabricated floating head covers shall be postweld heat treated when required by the Code or specified by the purchaser.

RCB-5.13 INTERNAL BOLTING

The materials of construction for internal bolting for floating heads shall be suitable for the mechanical design and similar in corrosion resistance to the materials used for the shell interior.

RCB-5.14 FLOATING HEAD BACKING DEVICES

The material of construction for split rings or other internal floating head backing devices shall be equivalent in corrosion resistance to the material used for the shell interior.

RCB-5.141 BACKING DEVICE THICKNESS (TYPE S)

The required thickness of floating head backing devices shall be determined by the following formulas or minimum thickness shown in Figure RCB-5.141, using whichever thickness is greatest.

BENDING

$$T = \left[\frac{(W)(H)(Y)}{(B)(S)} \right]^{1/2} \text{ For Style "A", "C" \& "D", inches}$$

$$\text{Metric } T = \left[\frac{(W)(H)(Y)}{(B)(S)} \right]^{1/2} \times 10^3, \text{ mm}$$

$$T = \left[\frac{2(W)(H)(Y)}{(B)(S)} \right]^{1/2} \text{ For Style "B", inches}$$

$$\text{Metric } T = \left[\frac{2(W)(H)(Y)}{(B)(S)} \right]^{1/2} \times 10^3, \text{ mm}$$

SHEAR

$$t = \frac{W}{(\pi)(Z)(S_s)}, \text{ inches}$$

$$\text{Metric } t = \frac{W}{(\pi)(Z)(S_s)} \times 10^6, \text{ mm}$$

where

A = Ring OD, inches (mm)	W = Design bolt load (as ref. in Code Appendix 2), lb. (kN)
B = As shown in Fig. RCB-5.141, inches (mm)	Y = From Code Fig. 2-7.1 using $K = A/B$
C = Bolt circle, inches (mm)	Z = Tubesheet OD, inches (mm)
H = $(C - B)/2$, inches (mm)	L = Greater of T or t , inches (mm)

S = Code allowable stress in tension (using shell design temperature), psi (kPa)

S_{br} = S of backing ring, psi (kPa)

S_{kr} = S of split key ring, psi (kPa)

S_{ts} = S of tubesheet, psi (kPa)

$$S_s = 0.8 S, \text{ psi (kPa)}$$

NOTES

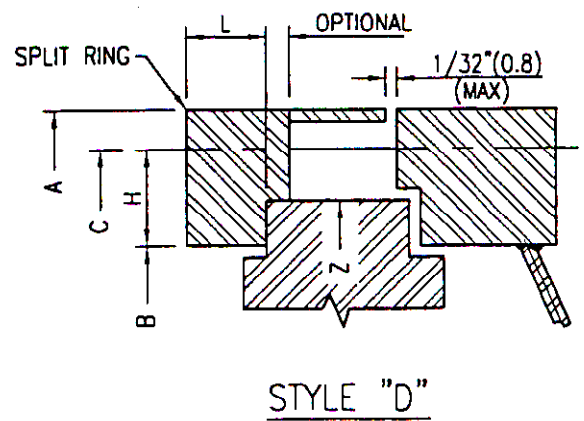
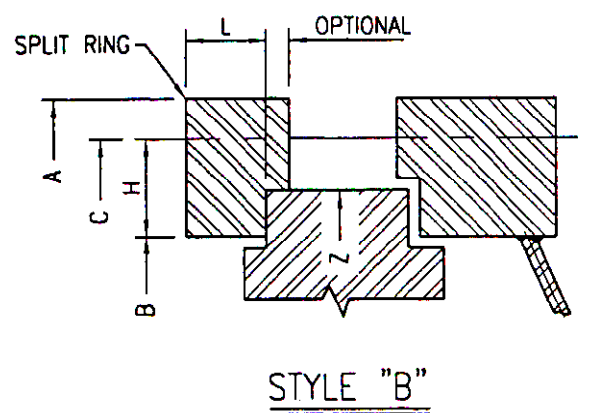
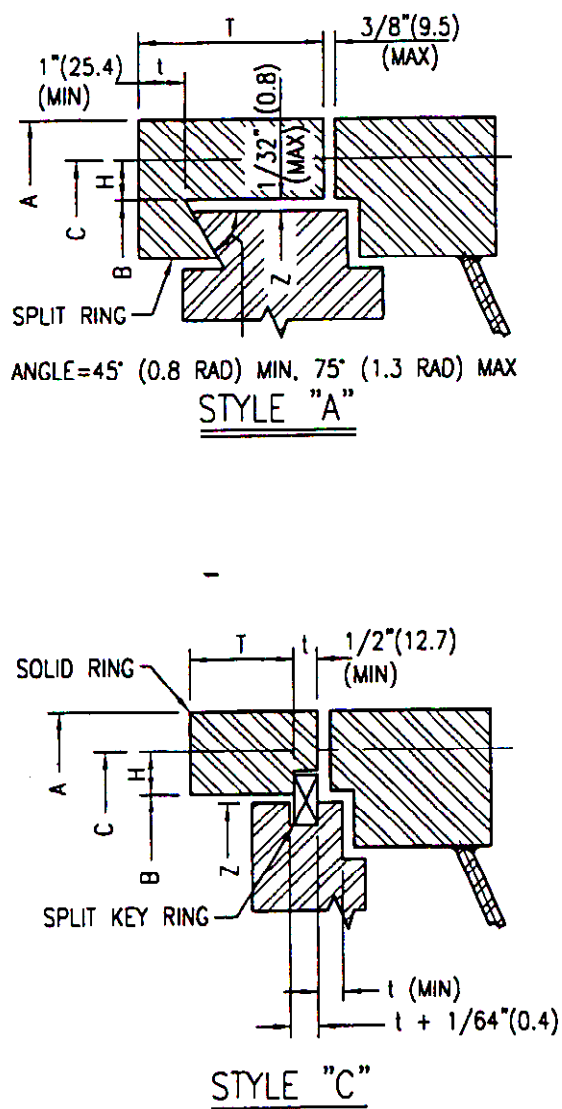
1. All references above are to ASME Code Section VIII, Division 1.

2. Caution: For styles "A", "B" & "D" check thickness in shear of the tubesheet if $S_{ts} < S_{br}$

3. Caution: Style "C" check thickness in shear of the tubesheet if $S_{ts} < S_{kr}$

See Figure RCB-5.141 for illustration of suggested styles. Other styles are permissible.

FIGURE RCB 5.141



RCB-5.15 TUBE BUNDLE SUPPORTS

When a removable shell cover is utilized, a partial support plate, or other suitable means, shall be provided to support the floating head end of the tube bundle. If a plate is used, the thickness shall equal or exceed the support plate thickness specified in Table R-4.41 or CB-4.41 as applicable for unsupported tube lengths over 60 inches (1524 mm).

RCB-5.16 FLOATING HEAD NOZZLES

The floating head nozzle and packing box for a single pass exchanger shall comply with the requirements of Paragraphs RCB-5.21, RCB-5.22 and RCB-5.23.

RCB-5.17 PASS PARTITION PLATES

The nominal thickness of floating head pass partitions shall be identical to those shown in RCB-9.13 for channels and bonnets.

RCB-5.2 OUTSIDE PACKED FLOATING HEADS (Type P)**RCB-5.21 PACKED FLOATING HEADS**

The cylindrical surface of packed floating head tubesheets and skirts, where in contact with packing (including allowance for expansion), shall be given a fine machine finish equivalent to 63 microinches.

RCB-5.22 PACKING BOXES

A machine finish shall be used on the shell or packing box where the floating tubesheet or nozzle passes through. If packing of braided material is used, a minimum of three rings of packing shall be used for 150 PSI (1034 kPa) maximum design pressure and a minimum of four rings shall be used for 300 PSI (2068 kPa) maximum design pressure. For pressures less than 150 PSI (1034 kPa), temperatures below 300° F (149° C), and non-hazardous service, fewer rings of packing may be used. Figure RCB-5.22 and Table RCB-5.22 show typical details and dimensions of packing boxes.

FIGURE RCB-5.22

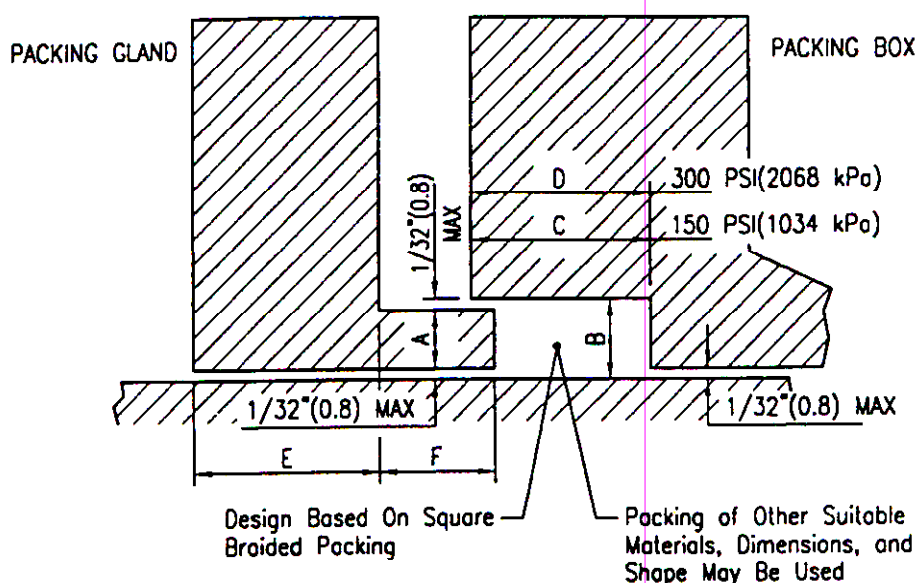


TABLE RCB-5.22

TYPICAL DIMENSIONS FOR PACKED FLOATING HEADS

150 PSI (1034 kPa) AND 300 PSI (2068 kPa) WITH 600 °F (316 °C) MAX. TEMP.

Dimensions in Inches

SIZE	A	B	C	D	E (MIN)	F	BOLTS	
							NO.	SIZE
6 - 8	3/8	7/16	1-1/4	1-5/8	1	3/4	4	5/8
9 - 13	3/8	7/16	1-1/4	1-5/8	1	3/4	6	5/8
14 - 17	3/8	7/16	1-1/4	1-5/8	1	3/4	8	5/8
18 - 21	3/8	7/16	1-1/4	1-5/8	1	3/4	10	5/8
22 - 23	3/8	7/16	1-1/4	1-5/8	1	3/4	12	5/8
24 - 29	1/2	9/16	1-3/4	2-1/4	1-1/8	1	16	5/8
30 - 33	1/2	9/16	1-3/4	2-1/4	1-1/8	1	20	5/8
34 - 43	1/2	9/16	1-3/4	2-1/4	1-1/8	1	24	5/8
44 - 51	5/8	11/16	2-1/8	2-3/4	1-1/4	1-1/4	28	5/8
52 - 60	5/8	11/16	2-1/8	2-3/4	1-1/4	1-1/4	32	5/8

Dimensions in Millimeters

SIZE	A	B	C	D	E (MIN)	F	BOLTS	
							NO.	SIZE
152-203	9.53	11.11	31.75	41.28	25.40	19.05	4	M16
229-330	9.53	11.11	31.75	41.28	25.40	19.05	6	M16
356-432	9.53	11.11	31.75	41.28	25.40	19.05	8	M16
457-533	9.53	11.11	31.75	41.28	25.40	19.05	10	M16
559-584	9.53	11.11	31.75	41.28	25.40	19.05	12	M16
610-737	12.70	14.29	44.45	57.15	28.58	25.40	16	M16
762-838	12.70	14.29	44.45	57.15	28.58	25.40	20	M16
864-1092	12.70	14.29	44.45	57.15	28.58	25.40	24	M16
1118-1295	15.88	17.46	53.98	69.85	31.75	31.75	28	M16
1321-1524	15.88	17.46	53.98	69.85	31.75	31.75	32	M16

Note: Nominal size of packing is same as dimension "A"